

# Heat to cool

Industrial Decarbonization



# Presentation



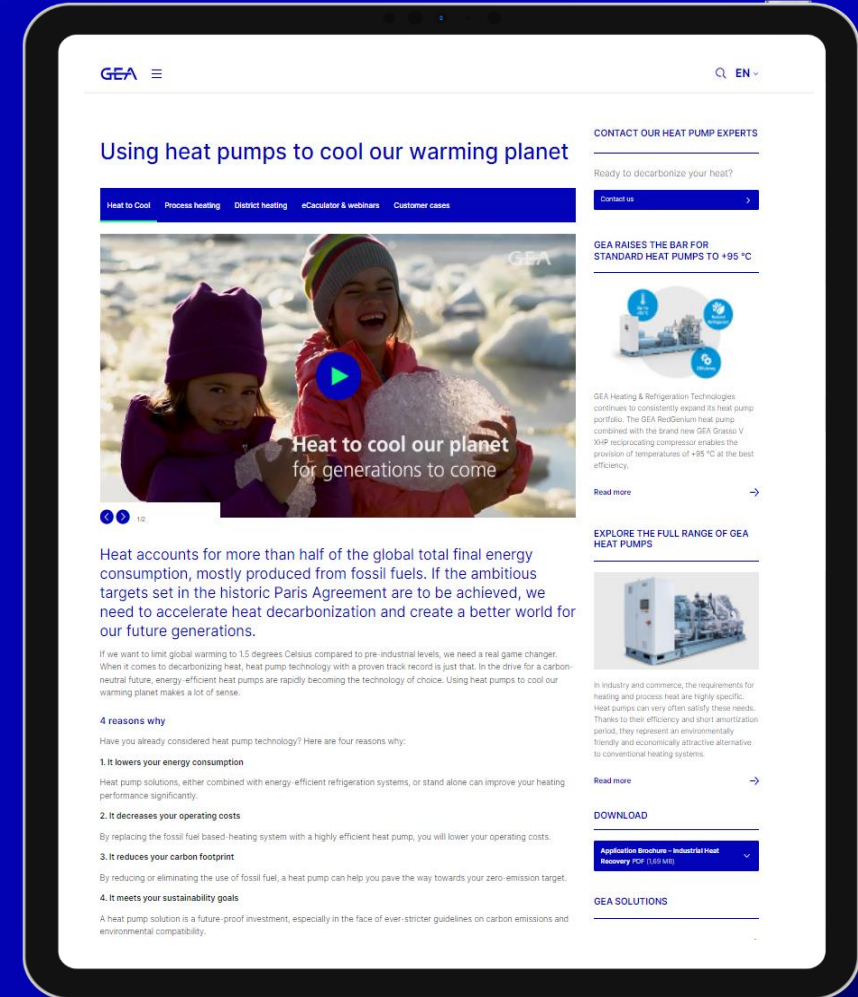
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- Mechanical Engineer
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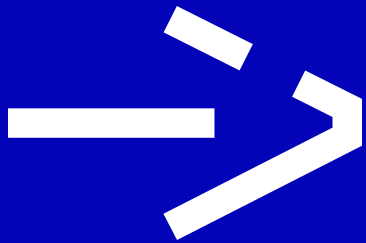
**German  
Robledo**












GEA.com/heat-to-cool



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# decarbonization

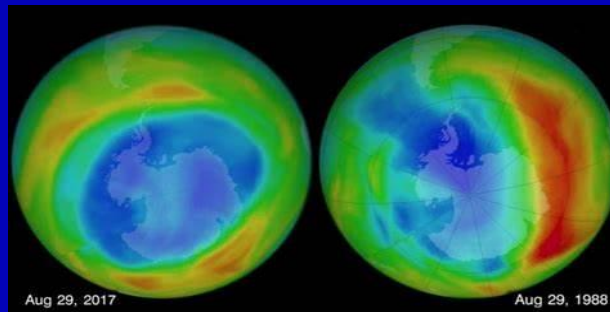
SUSTAINABILITY



# Why decarbonize?

## Ozone Layer

- In the last 30 years, human beings have made progress in stopping damage to the ozone layer.
- Recognition of the harmful effects of CFCs and other substances.
- It led to the signing of the Montreal Protocol in 1987: a landmark agreement for the phase-out of these substances.
- At the end of 2018, the UN confirmed in a scientific assessment that the ozone layer is recovering.



## Climate Change

- The Paris Agreement is an international treaty on climate change that was adopted on December 12, 2015 in Paris and entered into force on November 4, 2016.
- Their goal: to limit global warming to well below 2°C, preferably to 1.5°C, compared to pre-industrial levels.
- To achieve this goal, countries aim to reduce greenhouse gas emissions as much as possible, acronym Green House Gases (GHG).



TIME magazine and Statista have determined the world's most sustainable companies for 2024.

**GEA is one of the most sustainable companies in the world and is among the 33 best in the world and among the 3 best in Germany**

**1. Commitment to climate change**

**2. Several countries require labels on the product that show the carbon footprint produced, with tax effects and restrictions.**

**4. The consumer will have the option or purchase decision. The new generations are more aware.**

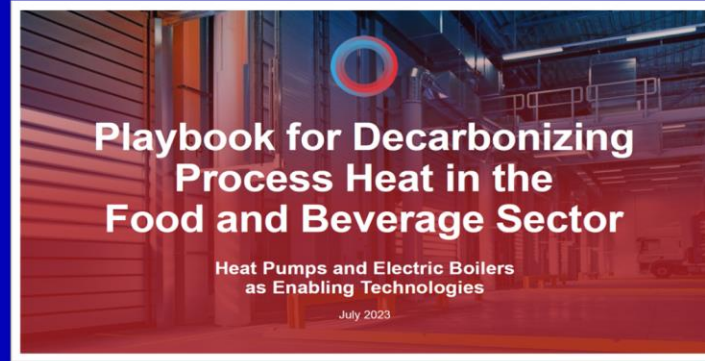
# Why decarbonize?

**3. Several countries require the carbon footprint of the manufacturer, also with tax effects and restrictions.**  
**CARBON TAX**

# How do we achieve this?

## FIRST

Prevent emissions through **RENEWABLE ENERGY** technologies such as wind, solar, geothermal, biomass, hydrogen.



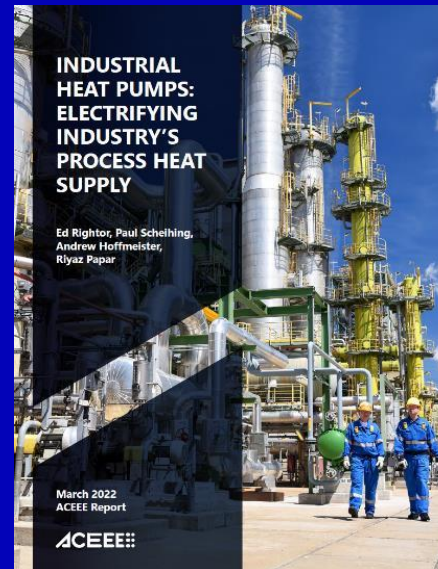
## SECOND

Find heating process technologies other than fossil fuel combustion.

**ELECTRIFY ALL HEATING PROCESSES.**

Using electricity as the way to generate or produce heat.

Fuel change. Electricity for fuel.



# The three scopes of Emissions

## Scope 1

### Direct Emissions:

All direct emissions, from the manufacturing process, your plant, what you produce in the product transformation.



## Scope 2

### Indirect emissions:

All forms of energy that you buy or use to be able to make the product transformation.



## Scope 3

### Associated emissions:

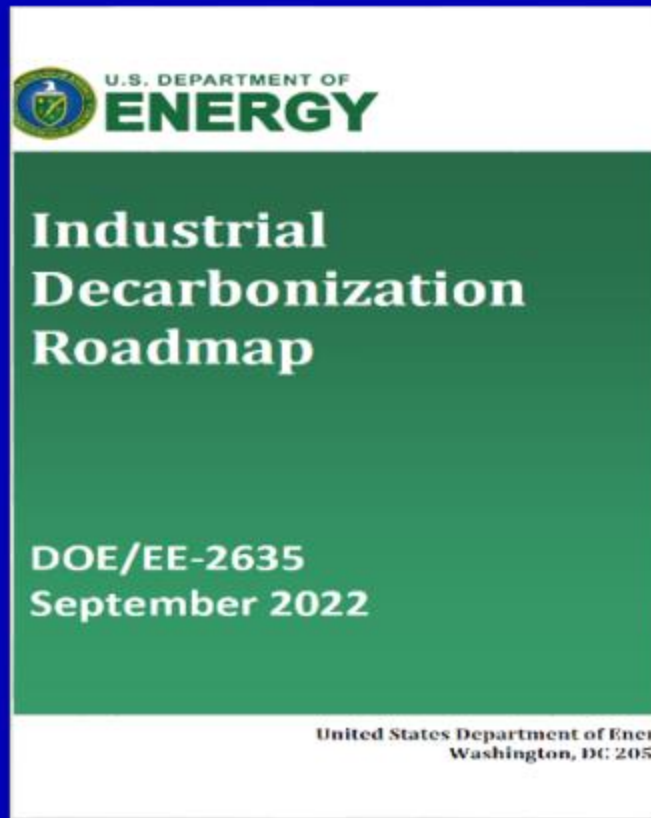
All forms of emissions produced in an associated manner. It can be your supply chain, the way your employees travel, your suppliers, etc.





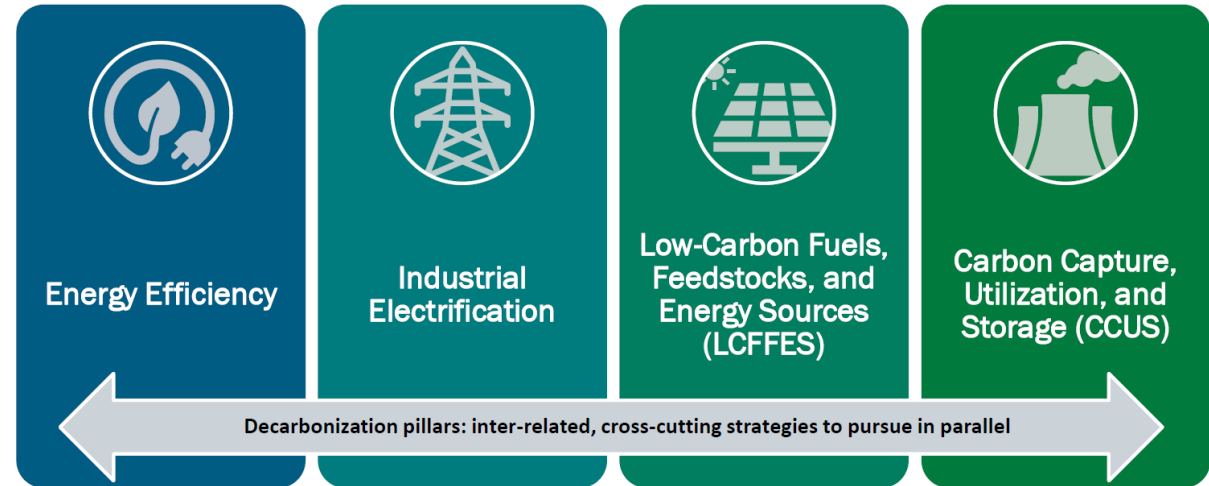
# Route to industrial decarbonization

Department of Energy of the United States of America



## U.S. DOE Industrial Decarbonization Roadmap

### Industrial Decarbonization Pillars



Iron & Steel



Chemicals



Food & Beverage



Petroleum Refining



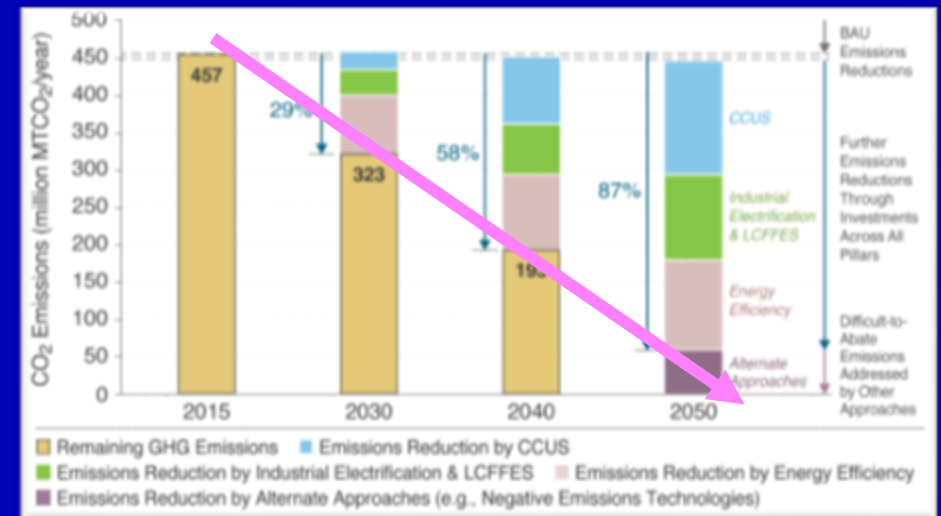
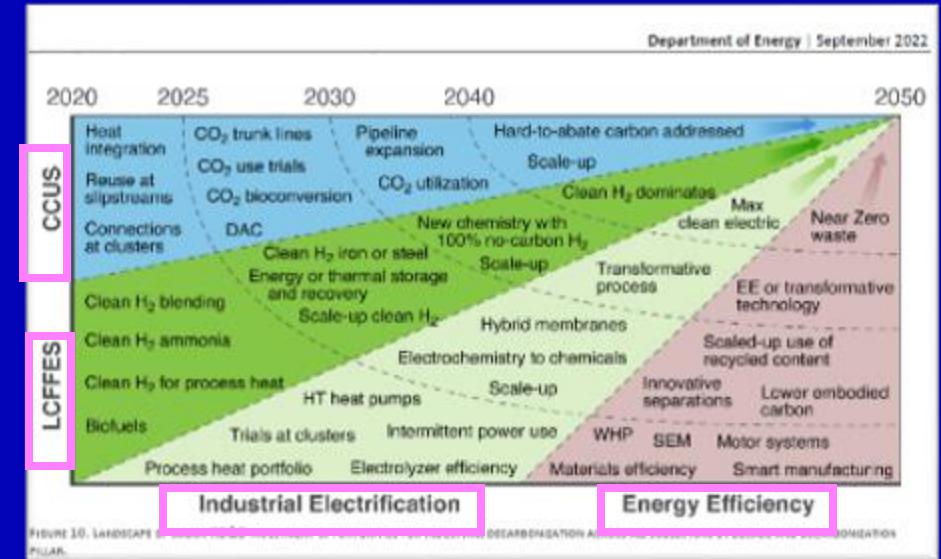
Cement

# The 4 pillars of the road to Decarbonization

1. **Energy Efficiency:** improve your current process.
2. **Electrification:** combustion heating technologies, e.g. by means of electricity.
3. **LCFFES (Low Carbon Fuel FeedStocks & Energy Sources)**  
Switching to low or zero carbon fuel: switching from fossil fuel to biomass or hydrogen in the combustion process.
4. **CCUS (Carbon Capture, Utilization and Storage):**  
Technologies that capture emissions before or after combustion and then use or inject them back into the earth.



Gradually implement one by one and expand until a 100% reduction is achieved.



# Heat pumps – Scopes of Emissions

**SCOPE 1**  
Heat Pump  
(Refrigerant Choice Option)



0 GWP Global Warming

0 DAMAGE OZONE LAYER

0 mol PFAs / TFAs Forever Chemicals



**SCOPE 1**  
Heat Pump  
(Heating Process)



Efficiency Improvement

Process Electrification

0 Fuel Consumption



**SCOPE 2**  
Heat Pump  
(Energy Consumption)



Process Electrification

More Electricity Consumption

Renewable energy



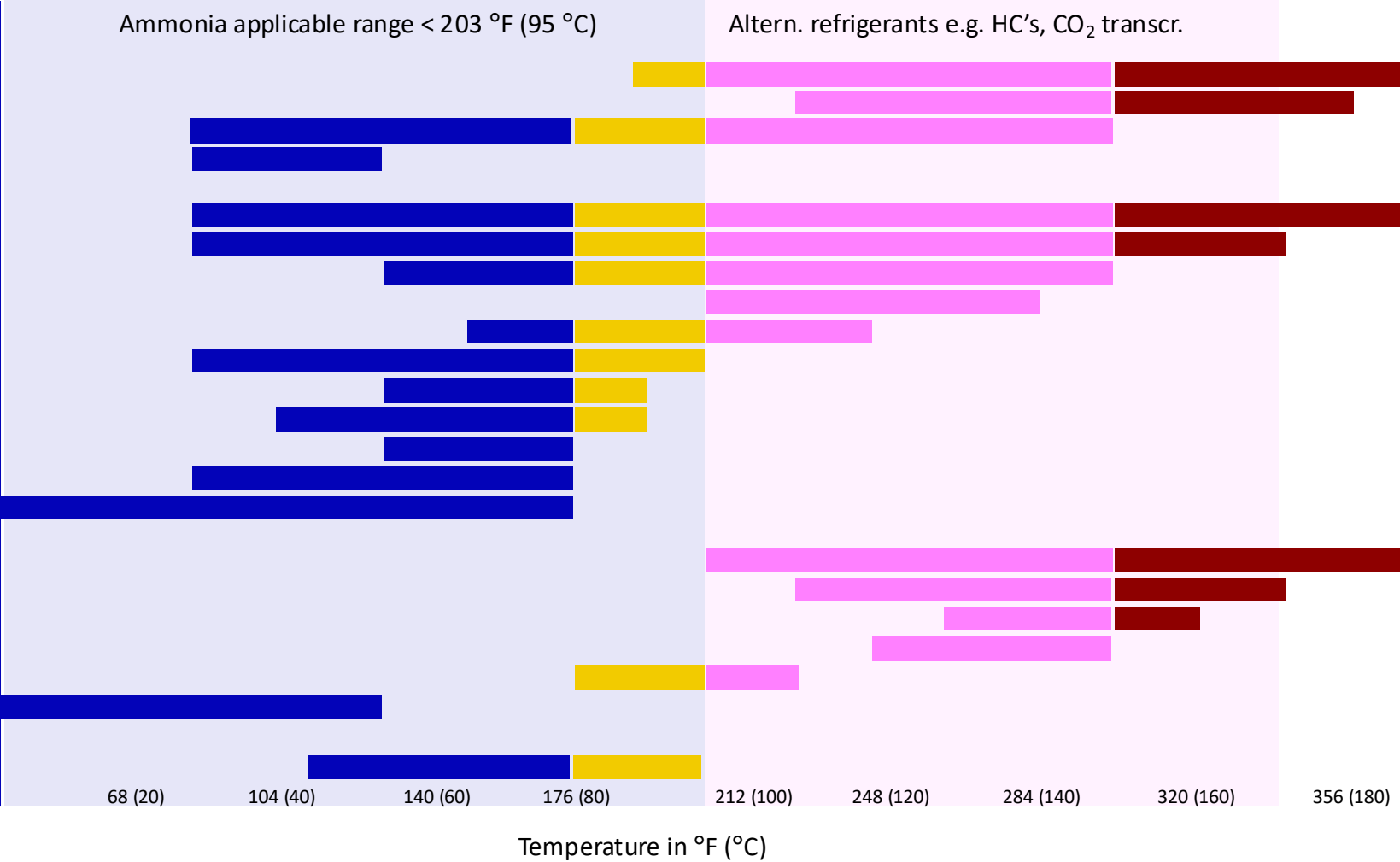
To achieve Carbon Reduction, it is achieved with the Use of Natural Refrigerant, Heat Pump and Renewable Energies

# Heat pump applications & temperatures

Heating needs in the process industry and for space heating:



- Drying
- Boiling
- Bleaching
- De-inking
- Drying
- Evaporation
- Pasteurization
- Sterilization
- Boiling
- Distillation
- Blanching
- Scalding
- Concentration
- Tempering
- Smoking
- Distillation
- Compression
- Thermoforming
- Concentration
- Boiling
- Bioreactions
- Heating



# Relevance of refrigerants

Features & benefits of the natural ammonia:



GWP = 0



High availability



High Efficiency



ODP = 0  
PFAS free



Low charges & costs



Safety

Example calculation with screw compressor <sup>1)</sup>:

NH<sub>3</sub> is  
40 % more  
efficient

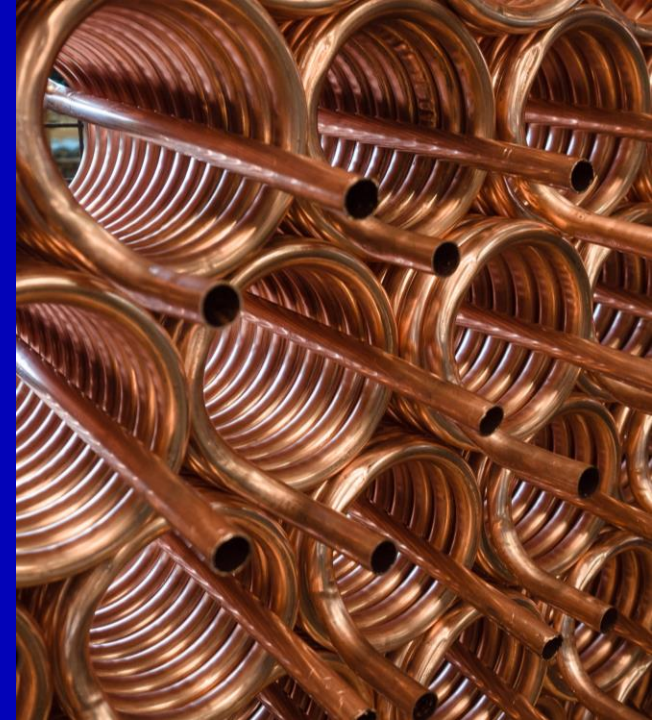
	COP in kW/kW	Heating Rating in MBH (kW) <sup>1</sup>	Vol. heating in kW/[m <sup>3</sup> /h]	GWP
R-717	3,43	17,490 (5125)	1,75	0
R134a	2,71	8,800 (2567)	0,88	1430
R152	2,95	10,200 (2817)	1,03	124
R1234yf	2,37	8560 (2510)	0,86	4
R1234ze	2,59	7510 (2201)	0,75	7
R1336mzzZ	3,00	1770 (518)	0,18	7
R600a	3,03	5870 (1720)	0,59	3
R515B	2,39	6810 (1996)	0,68	293

NH<sub>3</sub> provides  
twice the  
capacity

1) Z-type (2,927 m<sup>3</sup>/h swept volume, at +90/+77 °F (+32/+25 °C) heat source inlet/outlet, and +158/+194 °F (+70/+90 °C) heat carrier return/supply temperature.

# Thermal energy

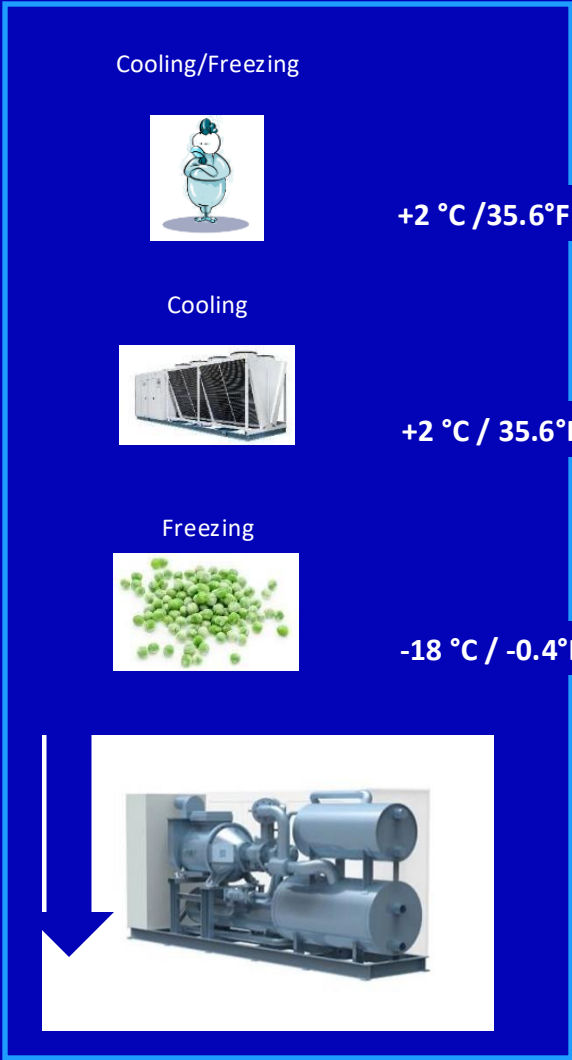
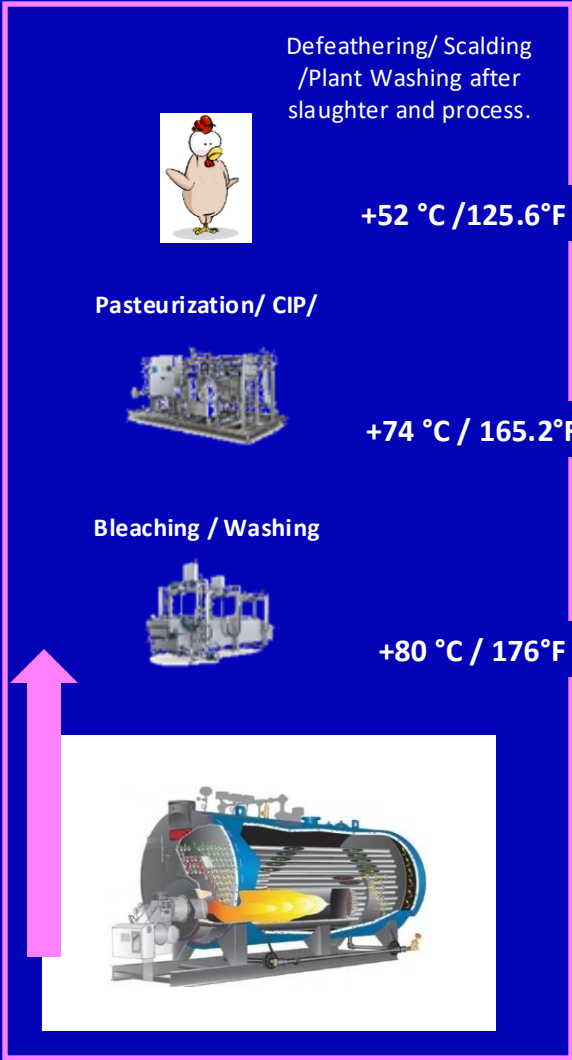
SUSTAINABILITY



# Understanding Thermal Energy Needs

## HEATING

## COOLING



## Final Product

Poultry Meat



+38 °C / 100.4°F

Dairy Beer Sodas Beverages



+2 °C / 35.6°F

Vegetables



+20 °C / 68°F



+52 °C /125.6°F

Pasteurization/ CIP/



+74 °C / 165.2°F

Bleaching / Washing



+80 °C / 176°F



+2 °C /35.6°F

Cooling



+2 °C / 35.6°F

Freezing



-18 °C / -0.4°F



+2 °C / 35.6°F



+2 °C / 35.6°F



-22 °C / -7.6°F



Same energy, but at different temperatures.

Heat: energy entering or being injected. Heat energy that goes out or is removed

# Available technology

LEVEL OF TECHNOLOGY AVAILABILITY

Commercial Now Available for  
T < 100°C

Prototype, pilot, demonstration

Still in development. Laboratory.

SECTOR	PROCESS	TEMPERATURES												°C	°F	TEMP RANGE			
		20	40	60	80	100	120	140	160	180	200								
		68	104	140	176	212	248	284	320	356	392								
Paper	Drying																	90-240°C	194-464°F
	Boiling																	110-180°C	230-356°F
	Bleaching																	40-150°C	104-302°F
	De-inking																	50-70°C	122-158°F
Food & Beverages	Drying																	40-250°C	104-482°F
	Evaporation																	40-170°C	104-338°F
	Pasteurization																	60-150°C	140-302°F
	Sterilization																	110-140°C	230-284°F
	Boiling																	70-120°C	158-248°F
	Distillation																	40-100°C	104-212°F
	Blanching																	60-90°C	140-194°F
	Scalding																	50-90°C	122-194°F
	Concentration																	60-80°C	140-176°F
	Tempering																	40-80°C	104-176°F
	Smoking																	20-80°C	68-176°F
	Chemical	Distillation																	100-300°C
Compression																		110-170°C	230-338°F
Thermoforming																		130-160°C	266-320°F
Concentration																		120-140°C	248-284°F
Boiling																		80-110°C	176-230°F
Bioreactions																		20-60°C	68-140°F
Automotive	Resin Molding																70-130°C	158-266°F	
Metal	Drying																	60-200°C	140-392°F
	Pickling																	20-100°C	68-212°F
	Degreasing																	20-100°C	68-212°F
	Electroplating																	30-90°C	86-194°F
	Phosphating																	30-90°C	86-194°F
	Chromating																	20-80°C	68-176°F
	Purging																	40-70°C	104-158°F
Plastic	Injection Molding																	90-300°C	194-572°F
	Pellets Drying																	40-150°C	104-302°F
	Preheating																	50-70°C	122-158°F
Mechanical Engineering	Surface Treatment																20-120°C	68-248°F	
Textiles	Cleaning																	40-90°C	104-194°F
	Coloring																	40-160°C	104-320°F
	Drying																	60-130°C	140-266°F
	Washing																	40-110°C	104-230°F
Wood	Bleaching																	40-110°C	104-230°F
	Glueing																	120-180°C	248-356°F
	Pressing																	120-170°C	248-338°F
	Drying																	40-150°C	104-302°F
	Steaming																	70-100°C	158-212°F
	Cocking																	80-90°C	176-194°F
Several Sectors	Staining																	50-80°C	122-176°F
	Pickling																	40-70°C	104-158°F
	Hot Water																	20-110°C	68-230°F
	Preheating																	20-100°C	68-230°F
	Washing /Cleaning																	30-90°C	86-194°F
Space Heating																	20-80°C	68-176°F	



# Combustion (boiler) vs. Heat pump (electricity)

## Boilers

They produce or generate heat.

Are Oversized.

They deliver temperatures above process.

Efficiencies between 80% and 90% (COP 0.8 and 0.9).

## Heat pumps

They do not produce heat, they move it.

It is selected for the required load and there is no oversizing.

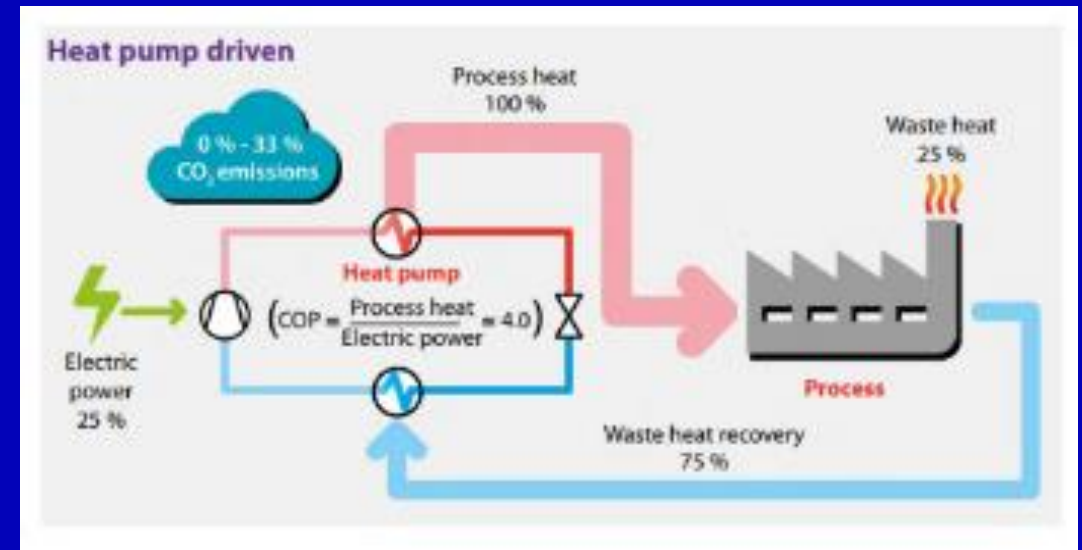
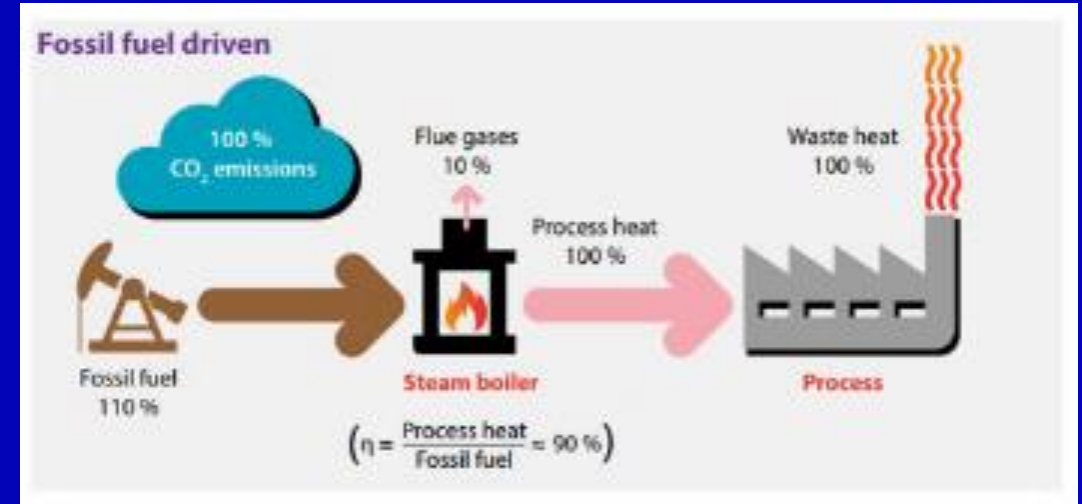
They don't waste energy.

It is selected for the required temperature and not above it.

Precision - Efficiency

Efficiencies between 300% and 1000% (COP 3.0 and 10.0)

They offer a double benefit: heating and cooling.



# Energy Cost Comparison / Spark Spread & Heat Pump Efficiency

Boiler Calculations								
Heat Capacity REQUIRED	kW	1500	5,115 MBH	HEAT PUMP COP	3.0			
Boiler Efficiency	%	80%	COP = 0.8					
Running hours	h / y	5,400	18 hours/day * 6 days * 50 weeks / year					
Energy Consumed	BOILER	1,875	HEAT PUMP	500	kW			
Natural Gas Burned	kWh/y	10,125,000	Electricity Used kW / y	2,700,000				

Assuming \$800 / kW (800\*1500)  
 Capital Cost of Heat Pump = \$1,200,000  
 does not include other associated costs

$$\text{Spark Gap} = \frac{\text{Electric Price} \left( \frac{\$}{\text{kWh}} \right)}{\text{Gas Price} \left( \frac{\$}{\text{kWh h eq}} \right)}$$

$$\text{Spark Gap} = \frac{\text{Electric Price} \left( \frac{\$0.10}{\text{kWh}} \right)}{\text{Gas Price} \frac{\$10}{\text{MMBtu}} * \left( \frac{1 \text{ MMBtu}}{293 \text{ kWh h}} \right)} = 2.9$$

Cost / kw/h	Electricity kW/h	Natural Gas Price \$/MMBtu	Natural Gas kW/h	Spark Gap (Ratio)	Boiler OPEX / y	Heat Pump OPEX / y	OPEX Diff / y	Return Of Investment (ROI) years
Lubbock, TX	\$ 0.0481	\$ 6.33	\$0.0216	2.2	\$218,700	\$ 129,870	\$ 88,830	14
Nevada	\$ 0.1047	\$ 10.84	\$0.0370	2.8	\$374,625	\$ 282,690	\$ 91,935	13
Trulock, CA	\$ 0.1129	\$ 13.60	\$0.0464	2.4	\$469,800	\$ 304,830	\$ 164,970	7
Fort Morgen, CO	\$ 0.0432	\$ 8.44	\$0.0288	1.5	\$291,600	\$ 116,640	\$ 174,960	7
Jerome, ID	\$ 0.0543	\$ 5.74	\$0.0196	2.8	\$198,450	\$ 146,610	\$ 51,840	23

\*ROI does not include other savings that may help reduce ROI, like water savings and others

	MW / h	MW / h
Lubbock, TX	\$ 48.10	\$ 21.60
Nevada	\$ 104.70	\$ 37.00
Trulock, CA	\$ 112.90	\$ 46.40
Fort Morgen, CO	\$ 43.20	\$ 28.80
Jerome, ID	\$ 54.30	\$ 19.60

Savings on Energy Costs

$$\text{Gas Price} - \left( \frac{\text{kw Price}}{\text{IHP COP}} \right)$$

Gas Price

Savings on Energy Costs	
≈	26%
≈	6%
≈	19%
≈	50%
≈	8%

Boiler Calculations								
Heat Capacity REQUIRED	kW	1500	5,115 MBH	HEAT PUMP COP	4.0			
Boiler Efficiency	%	80%	COP = 0.8					
Running hours	h / y	5,400	18 hours/day * 6 days * 50 weeks / year					
Energy Consumed	BOILER	1,875	HEAT PUMP	375	kW			
Natural Gas Burned	kWh/y	10,125,000	Electricity Used kW / y	2,025,000				

Assuming \$800 / kW (800\*1500)  
 Capital Cost of Heat Pump = \$1,200,000  
 does not include other associated costs

$$\text{Spark Gap} = \frac{\text{Electric Price} \left( \frac{\$}{\text{kWh}} \right)}{\text{Gas Price} \left( \frac{\$}{\text{kWh h eq}} \right)}$$

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Nevada	\$ 0.1047	\$ 10.84	\$0.0370	2.8	\$374,625	\$ 212,018	\$ 162,608	7
Trulock, CA	\$ 0.1129	\$ 13.60	\$0.0464	2.4	\$469,800	\$ 228,623	\$ 241,178	5
Fort Morgen, CO	\$ 0.0432	\$ 8.44	\$0.0288	1.5	\$291,600	\$ 87,480	\$ 204,120	6
Jerome, ID	\$ 0.0543	\$ 5.74	\$0.0196	2.8	\$198,450	\$ 109,958	\$ 88,493	14

\*ROI does not include other savings that may help reduce ROI, like water savings and others

	MW / h	MW / h
Lubbock, TX	\$ 48.10	\$ 21.60
Nevada	\$ 104.70	\$ 37.00
Trulock, CA	\$ 112.90	\$ 46.40
Fort Morgen, CO	\$ 43.20	\$ 28.80
Jerome, ID	\$ 54.30	\$ 19.60

Savings on Energy Costs

$$\text{Gas Price} - \left( \frac{\text{kw Price}}{\text{IHP COP}} \right)$$

Gas Price

Savings on Energy Costs	
≈	44%
≈	29%
≈	39%
≈	63%
≈	31%

**Spark Gap is the Electrical/\$Kw Fuel Cost Ratio \$kw Scoping Test (Proof of Savings Form)**

IHP COP	3.0
Gas Boiler Efficiency	80%
Efficiency Ratio ( IHP COP/ Boiler eff)	3.75

If the smallest Spark Gap, < 3.75, saves energy, gas is NOT convenient, electricity is.  
 If the Spark Gap equals, = 3.75, costs associated with the expense of gas or electricity would be even.  
 If the Spark Gap is greater, > 3.75, more is spent on electricity than on using gas, i.e., Gas is convenient.



The heat pump is more efficient than the boiler.

- Increasing the COP performance coefficient:
- OPEX improvement of the heat pump.
- Increases energy savings.
- Reduces ROI time.

# PISTON & SCREW EFFICIENCY

## PISTON

## Required Capacity 9 MW / 180°F

## SCREW

	WINTER	SUMMER
Heat Sink		
Process Fluid	Water	Water
Required Heating Capacity (KW)	5 X 1800	5 X 1800
Inlet Temperature (°F)	40	40
Outlet Temperature (°F)	180	180
Heat Source- Cascade Condenser		
General Data		
Chiller Model	RedGenium 950	RedGenium 950
Capacity per System (KW)	5 X 1800	5 X 1800
No. of Systems	5	5
Type of Compressor	Piston Model V950	Piston Model V950
	XHP	XHP
Compressor Motor BHP	432	432
Compressor Motor HP	500	500
Efficiency Summary		
COP - Coefficient of Performance (line)	5.13	5.78
COP - Coefficient of Performance (shaft)	5.59	6.29
Total electrical consumption (line), kW	351	311

Only Full Load Calculation		
	PISTON	SCREW
Running Hours per Year	5000	
TCO Period in Years	1	
Energy Costs per kW	\$0.12	
Capacity Heating kW	9000	
COP	5.13	4.27
Total unit Energy Consumption kWh	1755	2108
Total Energy Cost over Period	\$1,053,000	\$1,264,800
Savings	\$211,800	
PAYBACK years	3	

	WINTER	SUMMER
Heat Sink		
Process Fluid	Water	Water
Required Heating Capacity (KW)	4 X 2250	4 X 2250
Inlet Temperature (°F)	40	40
Outlet Temperature (°F)	180	180
Heat Source- Cascade Condenser		
General Data		
Chiller Model	RedAstrum RN	RedAstrum RN
Capacity per System (KW)	4 X 2250	4 X 2250
No. of Systems	4	4
Type of Compressor	Screw Model 230 GL	Screw Model 230 GL
Compressor Motor BHP	646.2	646.2
Compressor Motor HP	800	800
Efficiency Summary		
COP - Coefficient of Performance (line)	4.27	4.64
COP - Coefficient of Performance (shaft)	4.67	5.08
Total electrical consumption (line), kW	527	485

(Sell Price for 5 Units)\$3,141,550 USD

(Sell Price for 4 Units)\$ 2,508,533 USD

Price Difference \$ 633,017 USD BUT..... Payback on Piston becomes after 3 years resulting in more savings through whole lifecycle



# PISTON HEAT PUMP EFFICIENCY & SCREW HEAT PUMP EFFICIENCY

Boiler Calculations								
Heat Capacity REQUIRED	kW	9000	30,708 MMBH					
Boiler Efficiency	%	80%	COP = 0.8					
Running hours	h / y	5,000						
Energy Consumed	BOILER	11,250	HEAT PUMP	1754	kW			
Natural Gas Burned	kWh / year	56,250,000	Electricity Used kW / y	8,771,930				

**HEAT PUMP COP COP 5.13**  
**PISTON**  
(Sell Price for 5 Units) \$3,141,550 USD

Energy Savings 47,478,070 Kw/y

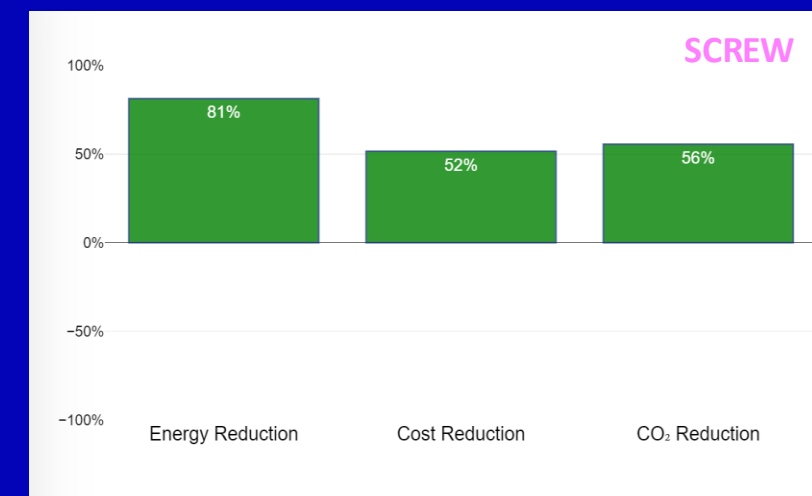
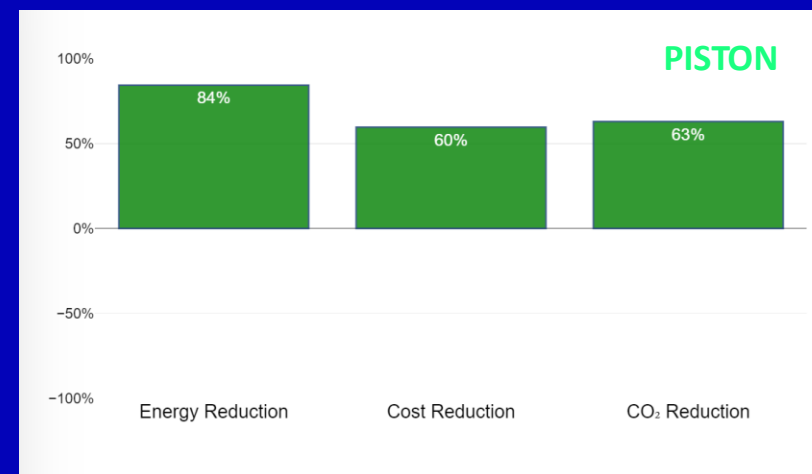
Cost / kw/h	Electricity kW/h	Natural Gas Price \$/MMBtu	Natural Gas kW/h	Spark Gap (Ratio)	Boiler OPEX / y	Heat Pump OPEX / y	OPEX Diff / y	Return Of Investment (ROI) years
	\$ 0.1200	\$ 13.60	\$ 0.0464	2.6	\$ 2,610,000	\$ 1,052,632	\$ 1,557,368	2

Boiler Calculations								
Heat Capacity REQUIRED	kW	9000	30,708 MBH					
Boiler Efficiency	%	80%	COP = 0.8					
Running hours	h / y	5,000						
Energy Consumed	BOILER	11,250	HEAT PUMP	2108	kW			
Natural Gas Burned	kWh / year	56,250,000	Electricity Used kW / y	10,538,642				

**HEAT PUMP COP COP 4.27**  
**SCREW**  
(Sell Price for 4 Units) \$ 2,508,533 USD

Energy Savings 45,711,358 Kw/y

Cost / kw/h	Electricity kW/h	Natural Gas Price \$/MMBtu	Natural Gas kW/h	Spark Gap (Ratio)	Boiler OPEX / y	Heat Pump OPEX / y	OPEX Diff / y	Return Of Investment (ROI) years
	\$ 0.1200	\$ 13.60	\$ 0.0464	2.6	\$ 2,610,000	\$ 1,264,637	\$ 1,345,363	2



Price Difference \$ 633,017 USD but ..... Energy Savings and CO2 Abatement will be diminished due to low COP

# Technologies Heat Pumps



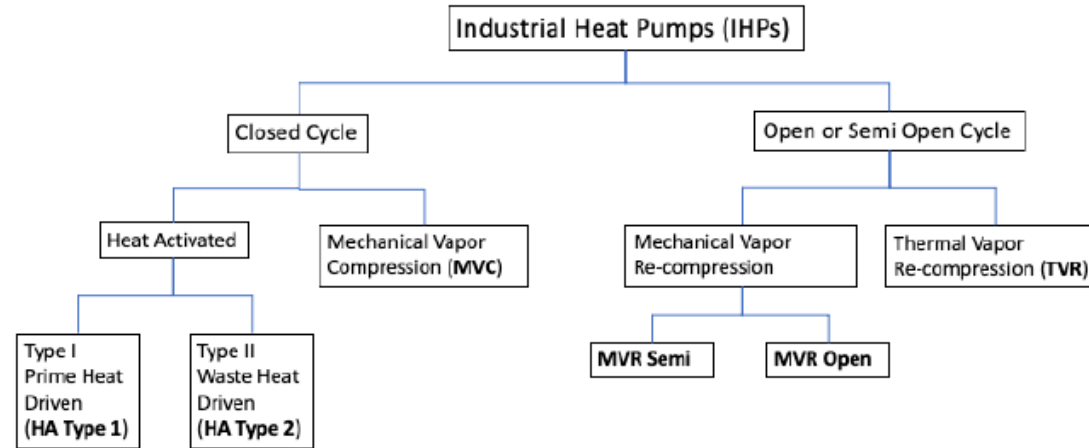
# Heat pump technologies

## CLOSED LOOP

HTHP

High-temperature heat pump

- Refrigerant Compression

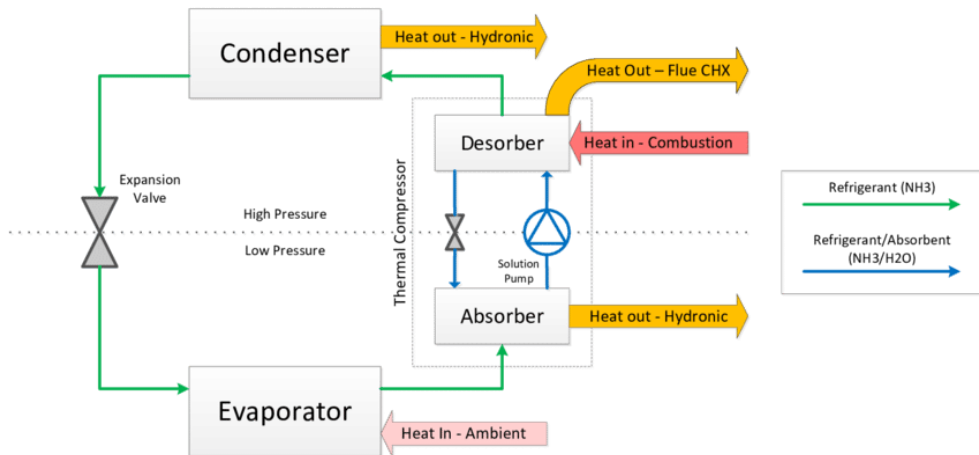


## OPEN CYCLE

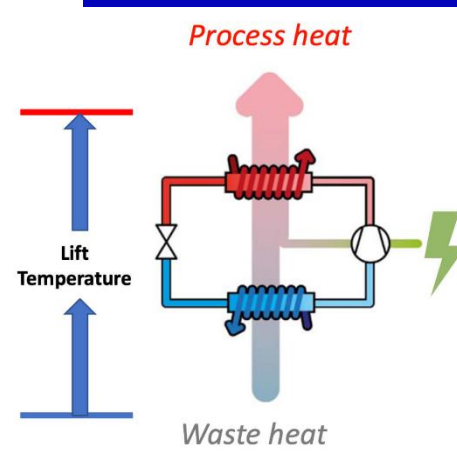
SGHP

Steam-Generating Heat Pump  
Vapor Recompression

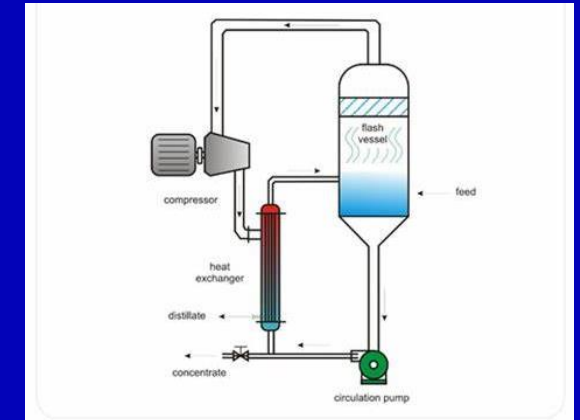
### Absorption cycles



### Refrigerant compression cycles



### Steam Recompression Cycles



# Application – Principle of Operation

## Compression Cycle

Process heat for various industries



Food, dairy and beverage production

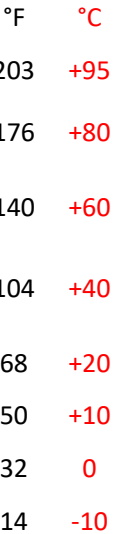
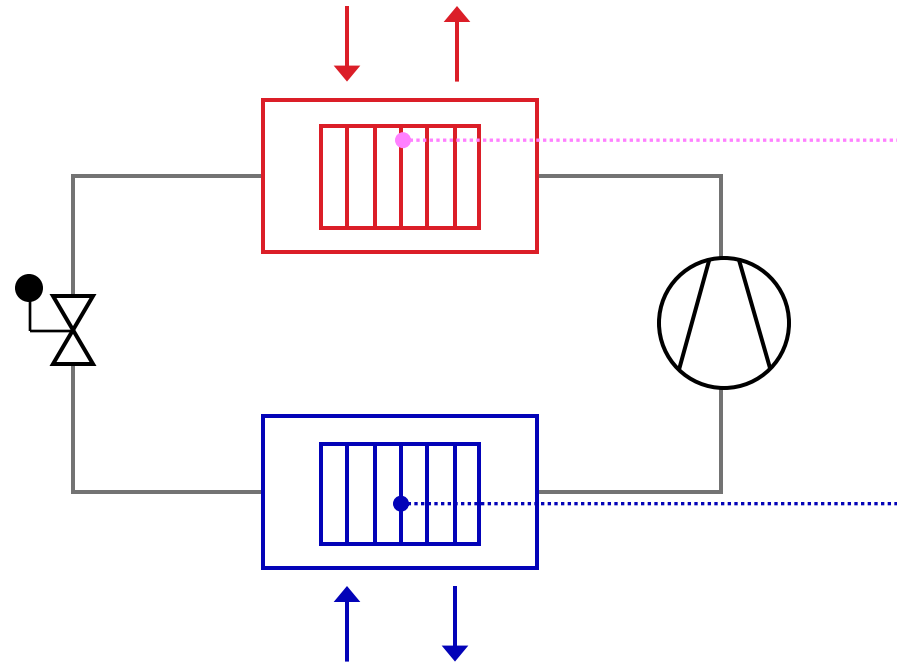
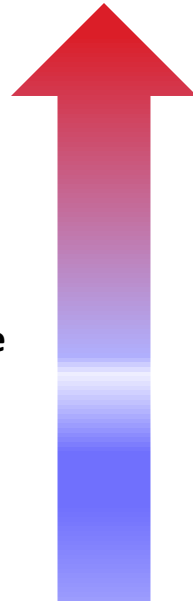


District/installation heating, hot water



Heat sink

By means of compression, rising to higher pressure = higher condensing = higher temperature



Process Heat/Waste Water



Cooling circuits

Heat source

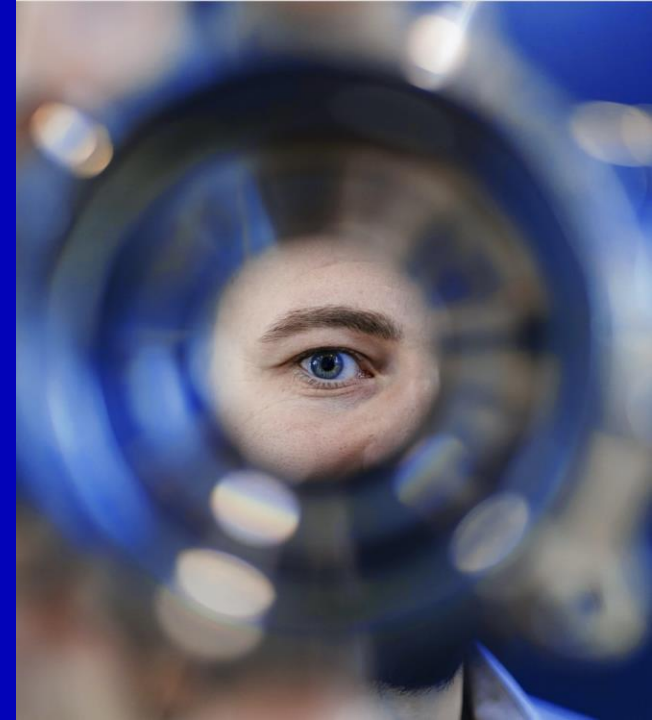
(liquid)



Environmental sources (sea, river, lakes, ...)

# HEAT PUMPS gea

SUSTAINABILITY





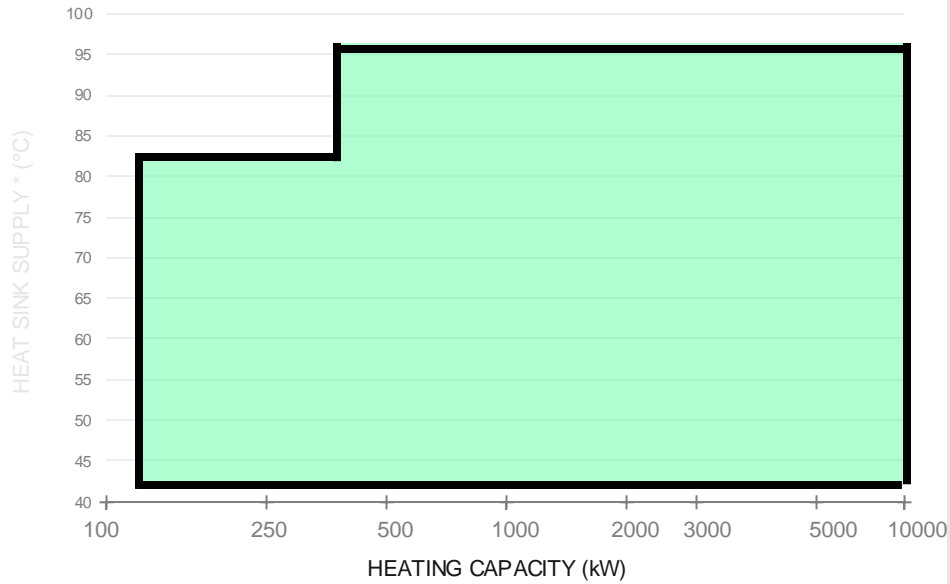
# Ammonia Heat Pump Example

GEA RedGenium



# GEA Portfolio in Heat Pumps – Capacity

## Temperature Application Diagram



The highlighted area shows the range of supply temperatures for heating demand and heat capacity at the ambient heat source level.



### RedGenium

Piston Heat Pump

11 types

Up to +95 °C / 203°F

- 150 – 3,500 kW
- 511 – 11,945 MBH

**Approach:**

Higher supply temperatures

Best-in-class efficiency

Lower power consumption

### RedAstrum

Screw Type Heat Pump

7 types

Up to +85 °C / 185°F

- 500 – 3,000 Kw
- 1706 – 10,238 MBH

**Approach:**

Low installation footprint  
High differential pressures

Focused for high differential temperature between heat source and heat reservoir

### Blu-Red Fusion

Chiller + Heat Pump

Multiple types

Up +95 °C / 203°F

- 500 – 3,500 kW
- 1706 – 11,945 MBH

**Approach:**

Combined cooling and heating

Maximum efficiency  
Flexibility  
Simultaneous or variable cooling and heating possible.

### Custom

Custom Heat Pumps  
All compressors

Up to +95 °C / 203°F

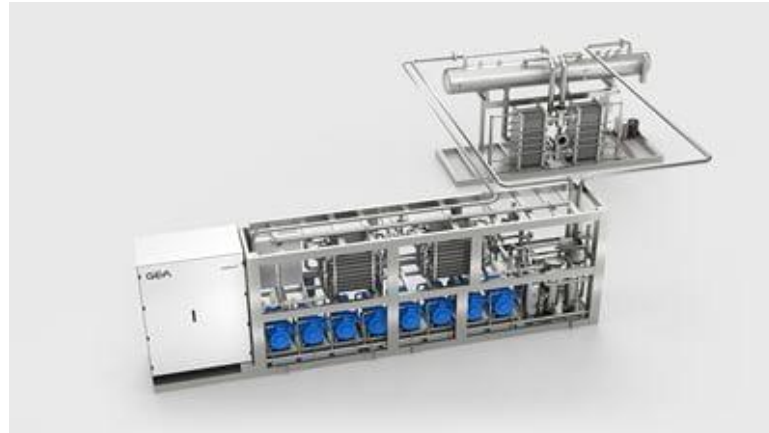
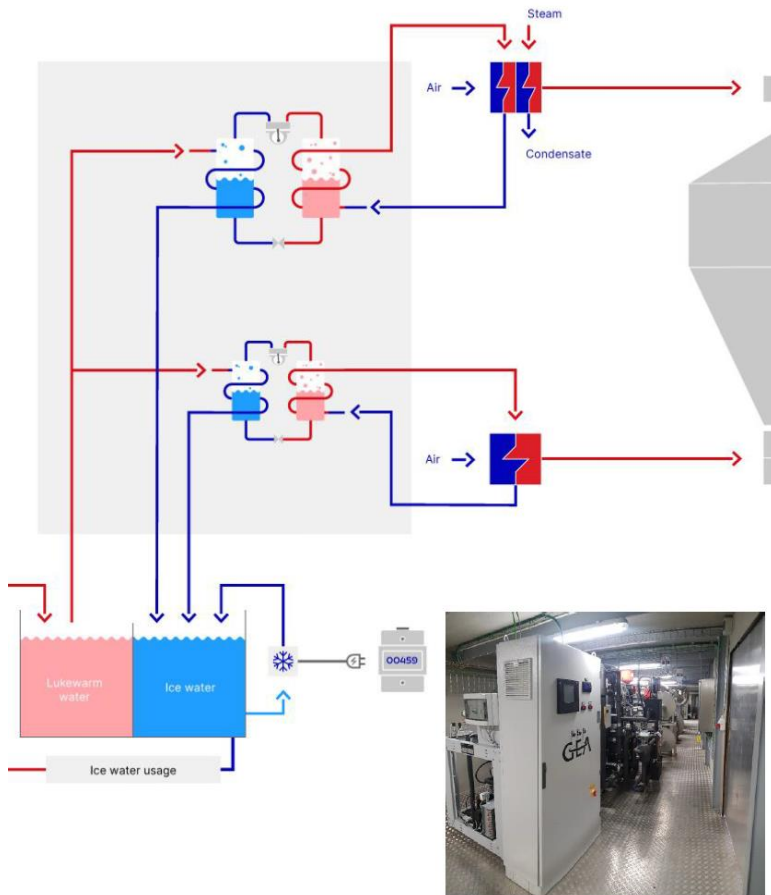
- 250 – 10,000 Kw
- 853 – 34,129 MBH

**Approach:**

High Heat Capacity  
Many flexible design and configuration options

# ADD COOL

## Spray drying



- Spray drying is an industry-standard method for making high-quality, stable powder products.
  - The production of the hot air used by the atomization tower usually uses energy generated by fossil fuels.
  - To make spray drying more sustainable, GEA integrates heat pumps
- ADDCOOL GEA uses CO<sub>2</sub> Refrigerant heat pumps to preheat air up to temperatures of 120°C
- At the same time, 2°C cold water is generated that can be supplied to the existing cold water network to reduce energy consumption
  - Drying Operation and Product Quality Are Not Affected

# GEA Heat Pump References

Some global examples of applications

Thermal Districts(CND)  
2x 2-stage heat pumps

Foods (UK&IRL)  
7x GEA Red heat pumps

Pharmaceutics (FRA)  
1x GEA RedAstrum

DT Berlin Neukoelln DH (GER)  
2x GEA RedGenium

Nestlé food factory (SER)  
3x GEA RedGenium

SANITIZE PLANT(BHR)  
1x GEA RedGenium

Confiterie (BRASIL)  
1x GEA custom recip hp

**By 2024 GEA HRT has  
installed over 200 heat  
pumps**

# GEA Heat Pumps References

## North America

1x RedGenium 950 (K)  
5,800 MBH / 1.7 MW

1x RedGenium 550 (K)  
3,412 MBH / 1 MW

1x RedGenium 950 (K)  
7,000 MBH / 2.05 MW

2x RedGenium 950 (W)  
14,672 MBH / 4.3 MW total

2x RedGenium 950 (K)  
14,332 MBH / 4.2 MW total

2x 2-stage heat pumps  
13,650 MBH / 4 MW total

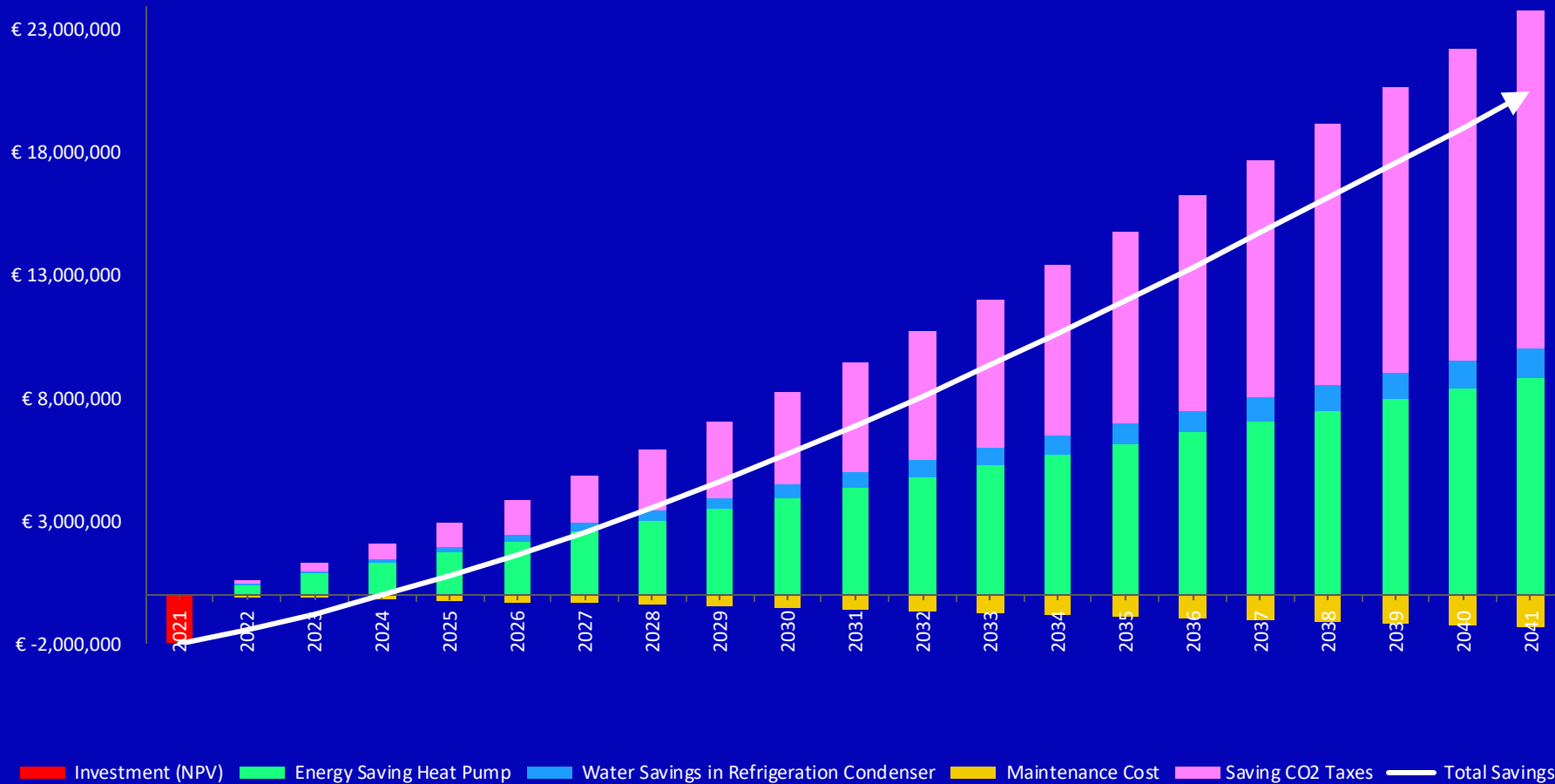
- Applications**
- Dairy
  - District Thermals
  - Brewery
  - Food

The map shows the location of current heat pump projects for GEA North America. The heat pumps may be at different stages (in operation, commissioning, in production).

# Total Cost Ownership - TCO



## INNOCENT - The World's First Climate Neutral Juice Factory



Total savings  
\$ 20.500.386

CO2 emissions avoided 103,158 tons (green electricity)

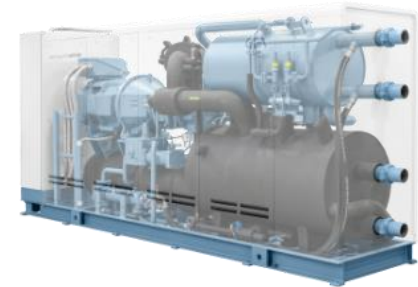
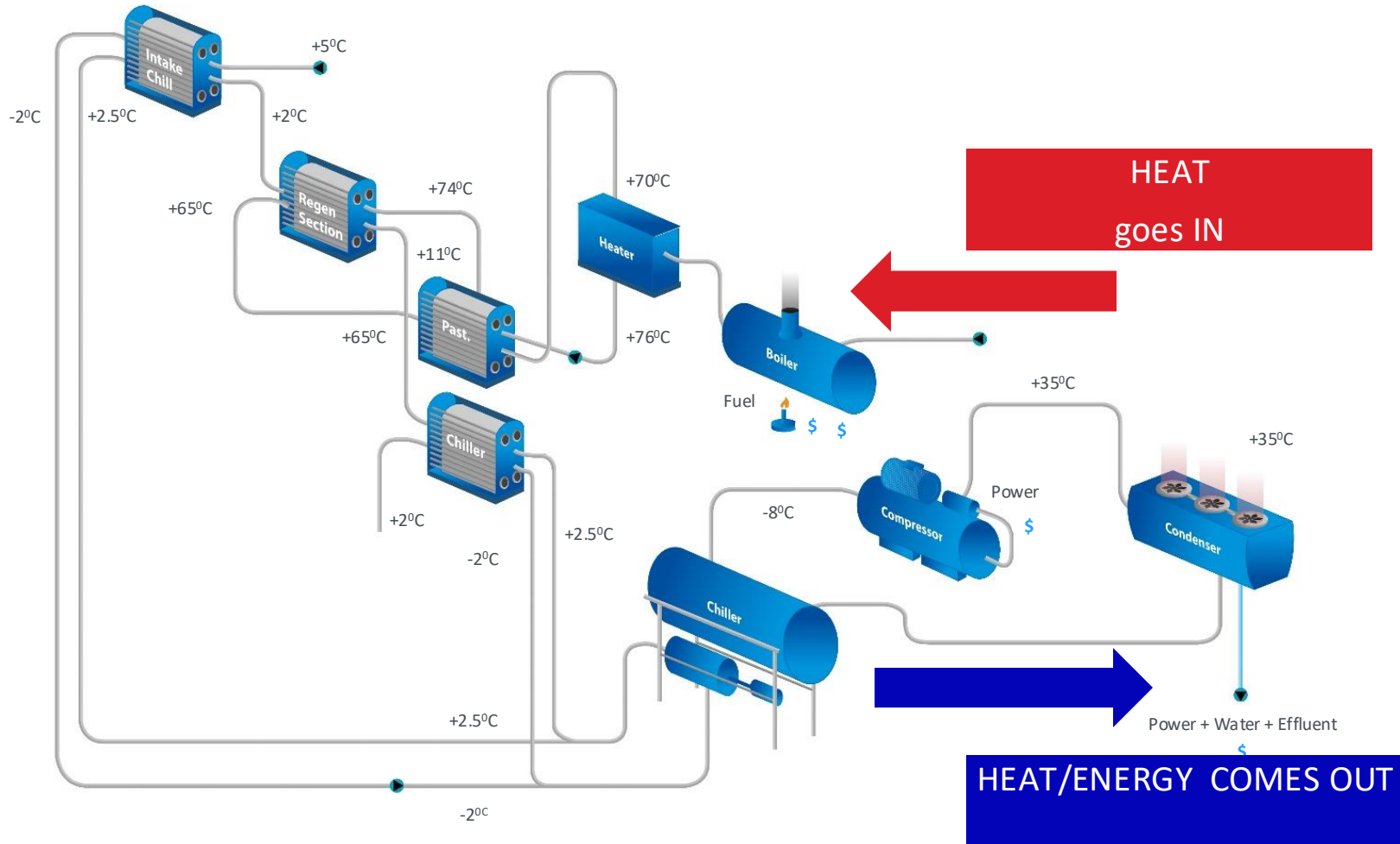
- Fuel price \$ 0.207 /Nm3
- Electricity price \$0.052 /kWh
- CO2 emits. (\$/ton/y)\$ 30
- Annual energy cost increases acc. Polynomial
- Annual water cost increases 0%
- Annual maintenance cost increases 2%
- Annual CO2 tax increases acc. Polynomial

# Application examples



# Example in dairy products

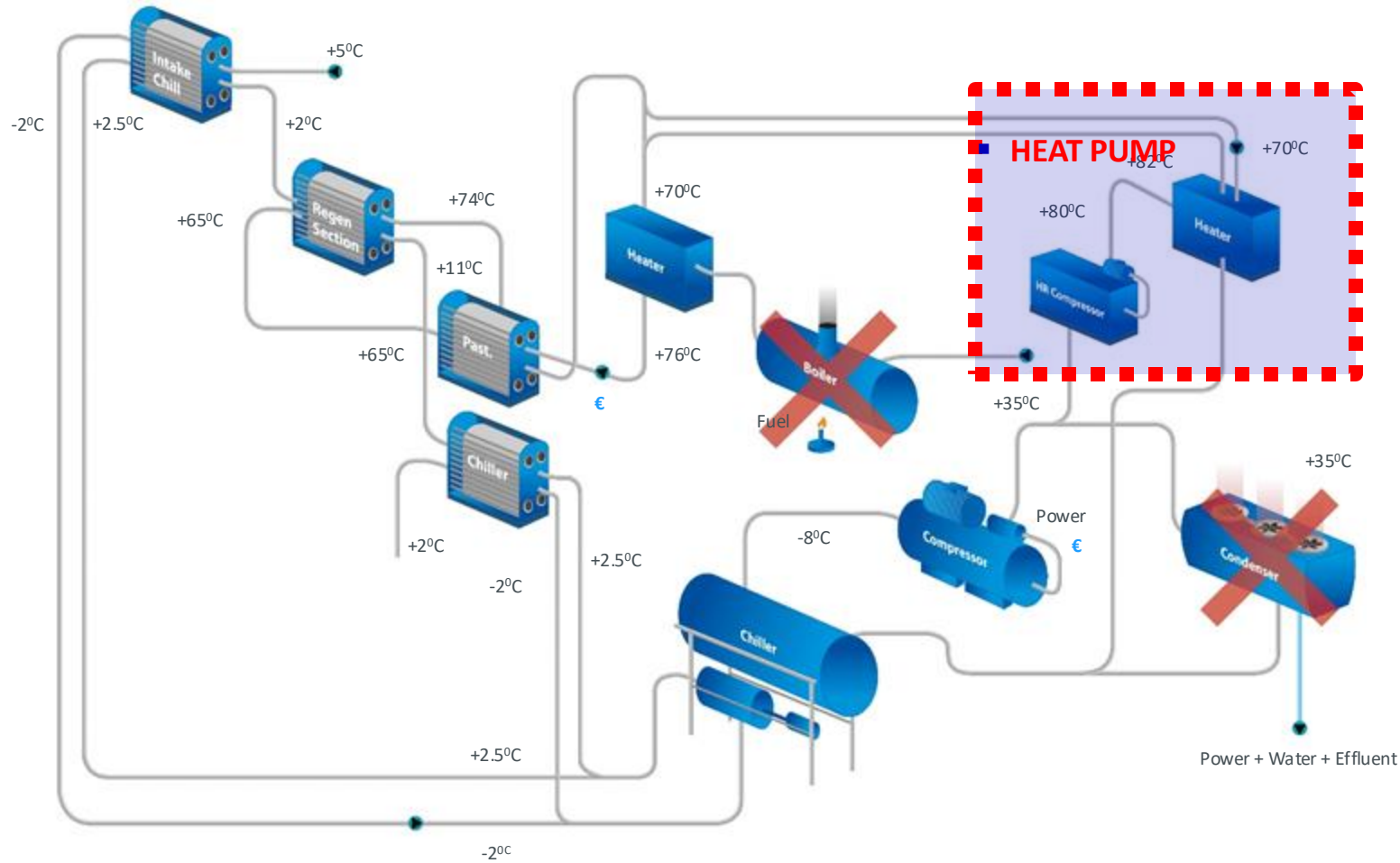
## Cooling and heating





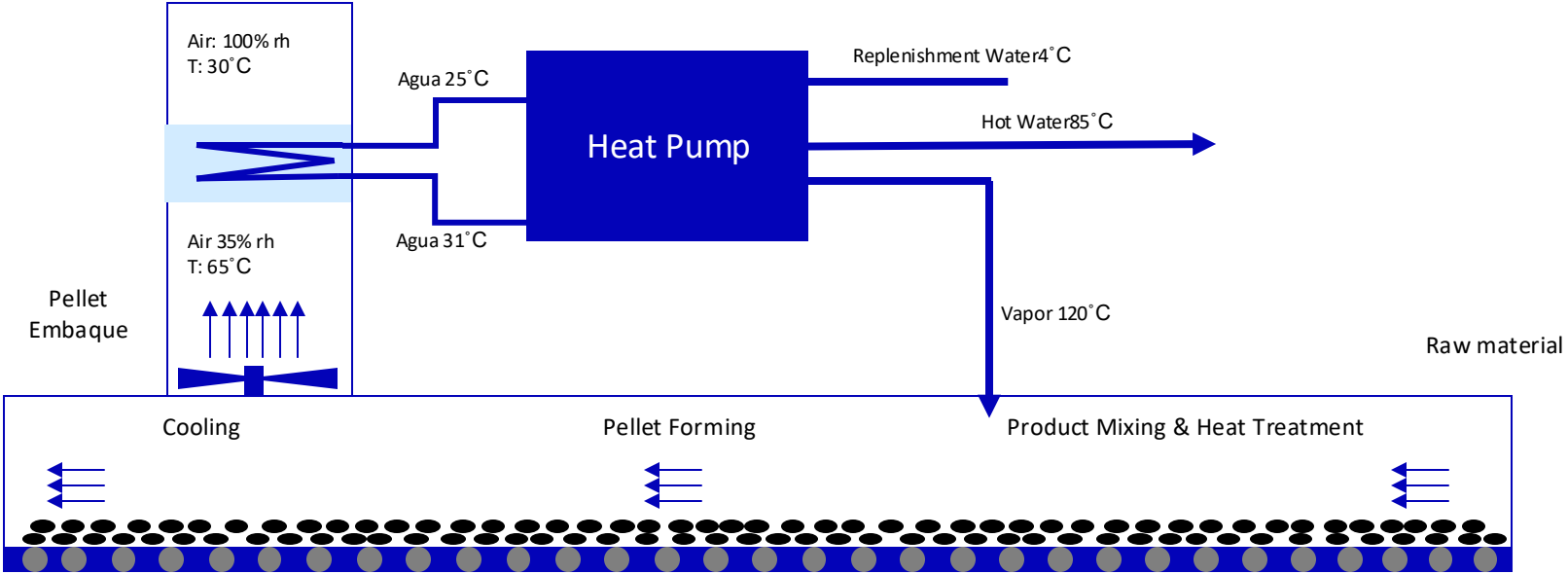
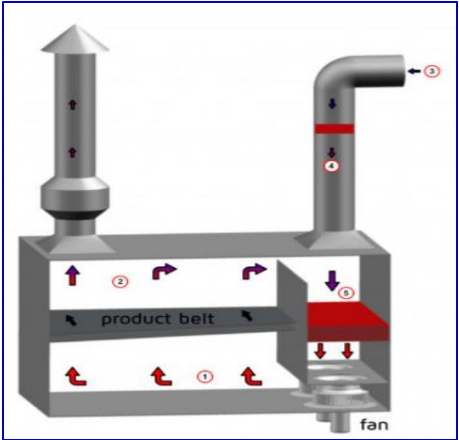
# Example in dairy products

## Cooling and heating

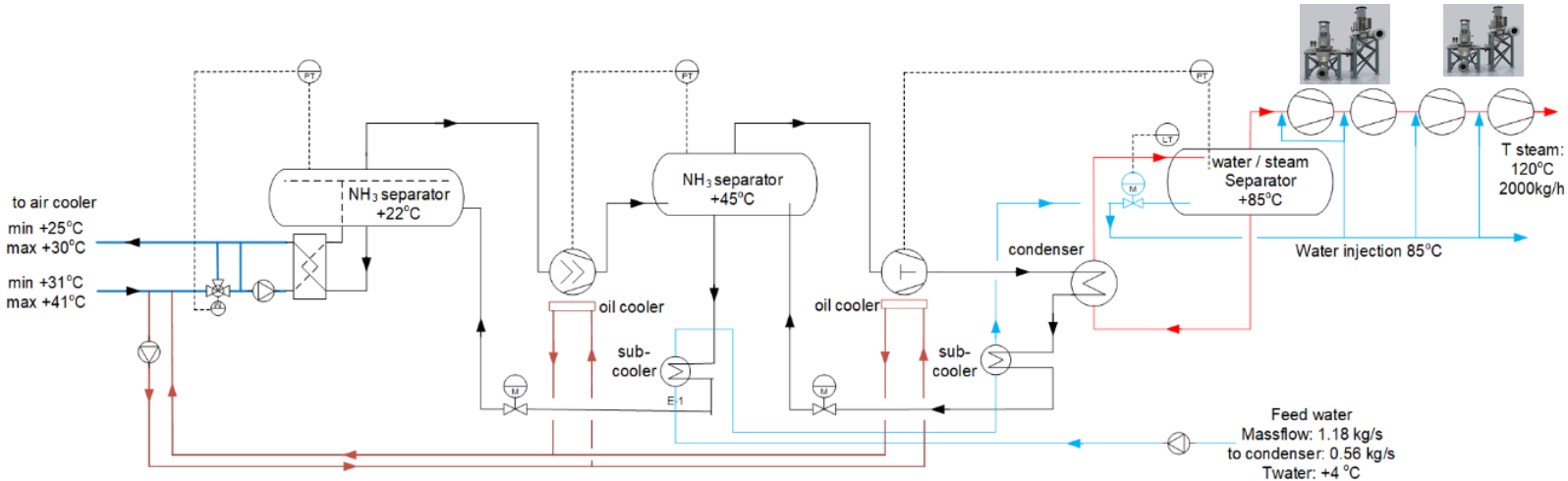
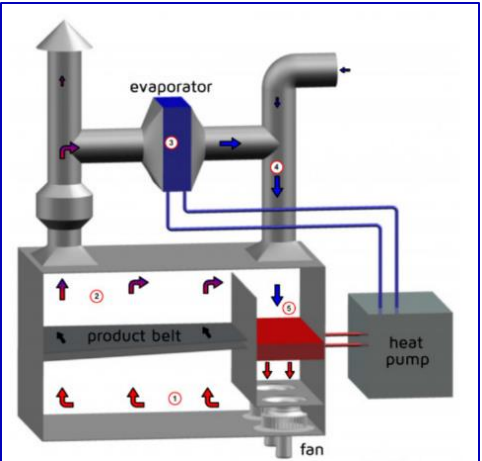


# Example in drying

CONVENTIONAL DRYING

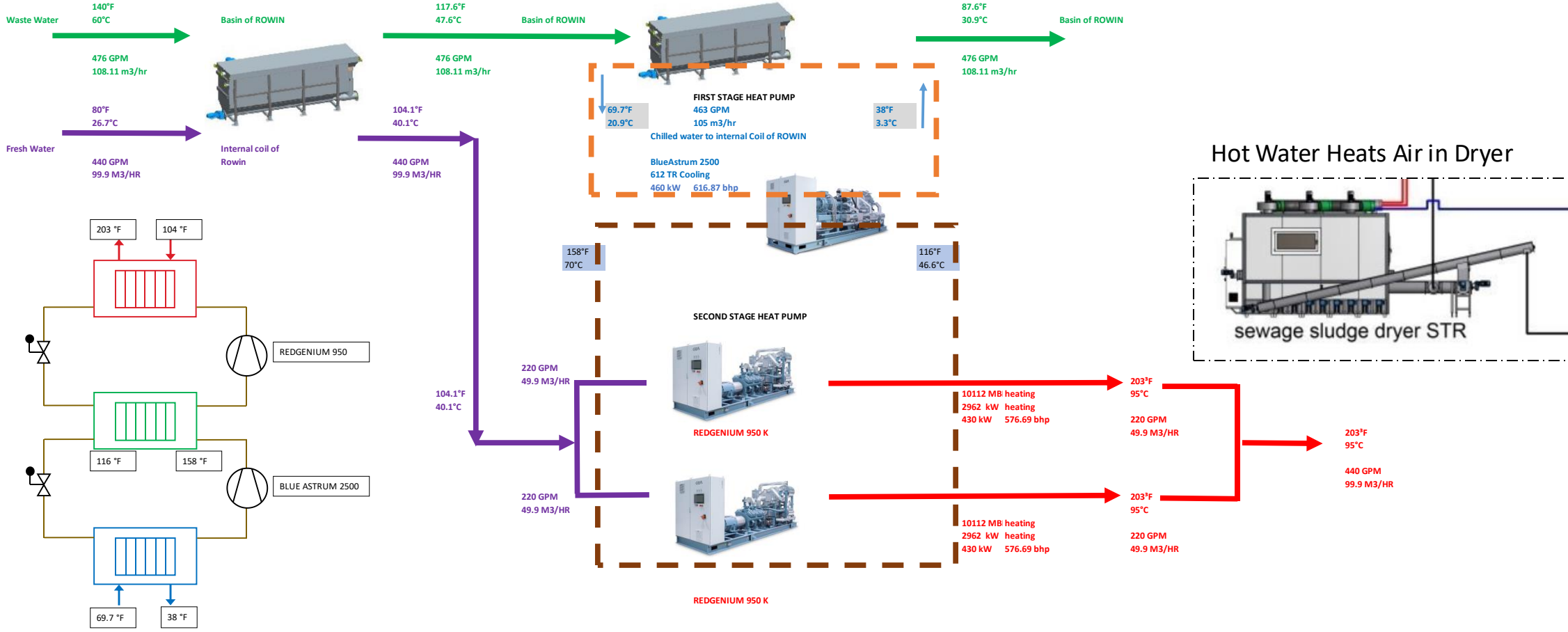


DRYING VIA HEAT PUMP



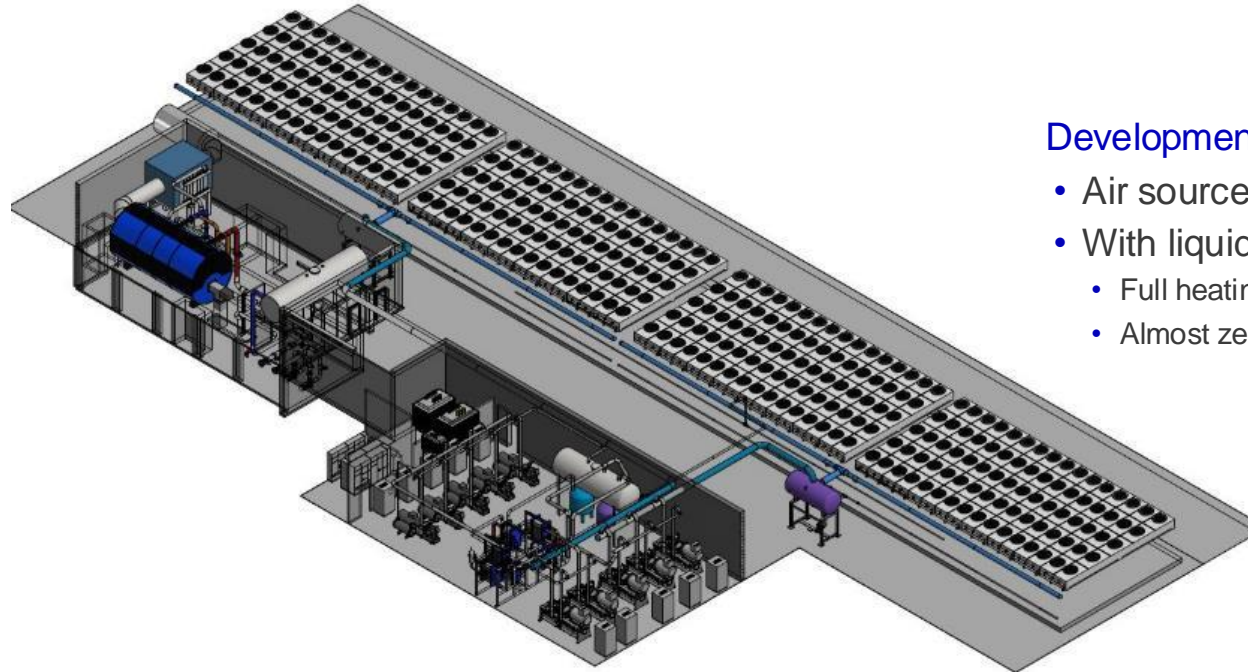
# Example Wastewater / Water Treatment / Sewage Water

Heating or Drying by means of heat pumps



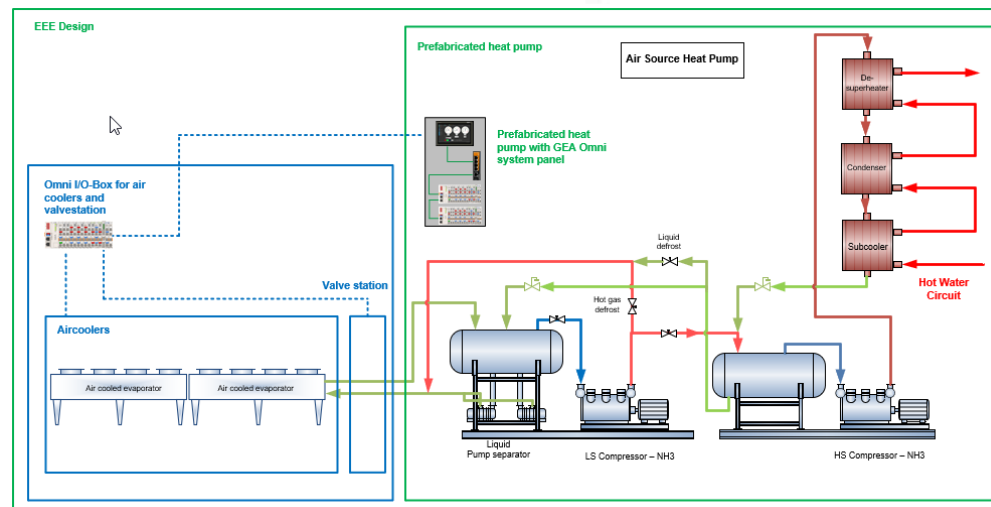
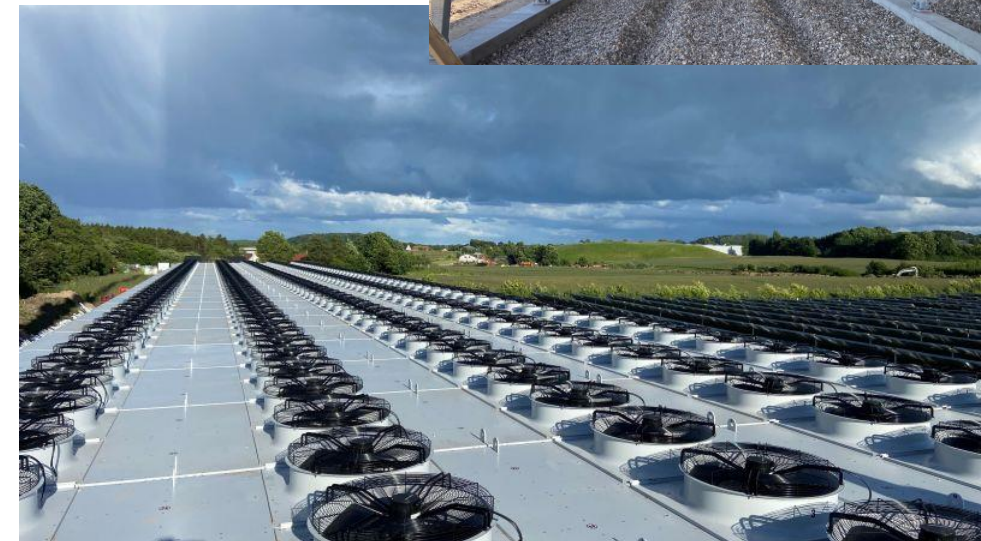
# ASHP – AIR SOURCE HEAT PUMP

Illustration of generic 10MW airtsource heat pump

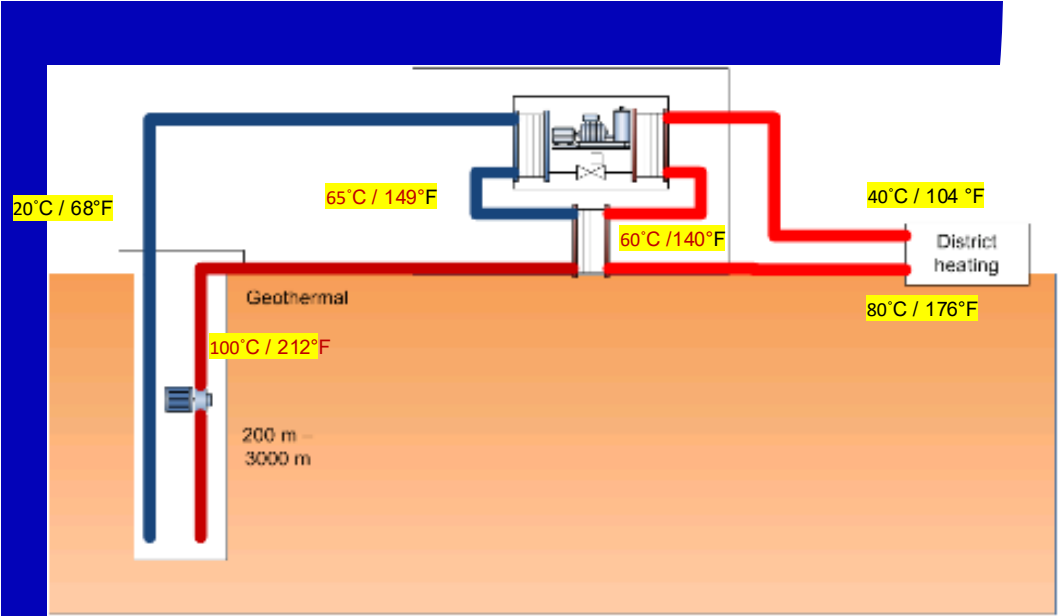


## Development project

- Air source heat pump with direct ammonia
- With liquid ammonia defrost
  - Full heating capacity during defrost period
  - Almost zero energy required for defrost

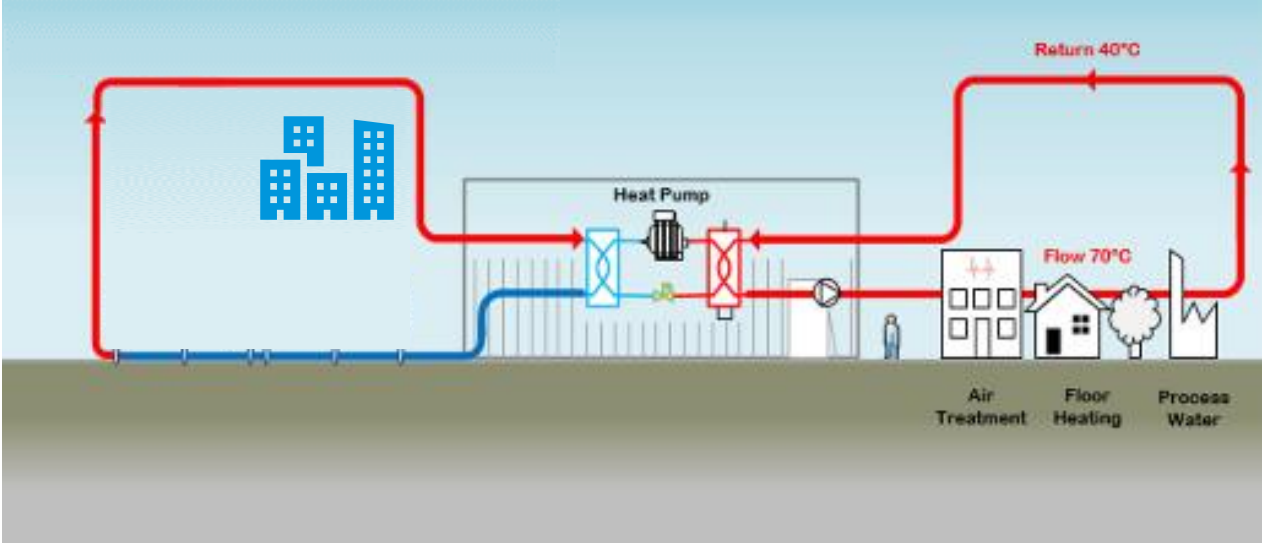


# GSHP - GEOTHERMAL SOURCE HEAT PUMP



DEEP GEOTHERMAL HEAT

COMBINED HEATING AND COOLING



# Decarbonize steam

SUSTAINABILITY



# Steam / Heat Pump / n-Pentane Refrigerant (R601) / Demo Site / Belgium

## Sugar Production Process Plant

### Demo-site 2

**COP<sub>heating</sub> = 2.9**

**Process Heat:**  
3.4 bar<sub>a</sub> steam for concentration of sugar juices

~3500 kW @ 138°C

~1250 kW

~2500 kW @ 76°C

**Source Heat:**  
Vacuum steam from multi-effect evaporator

**Process:**

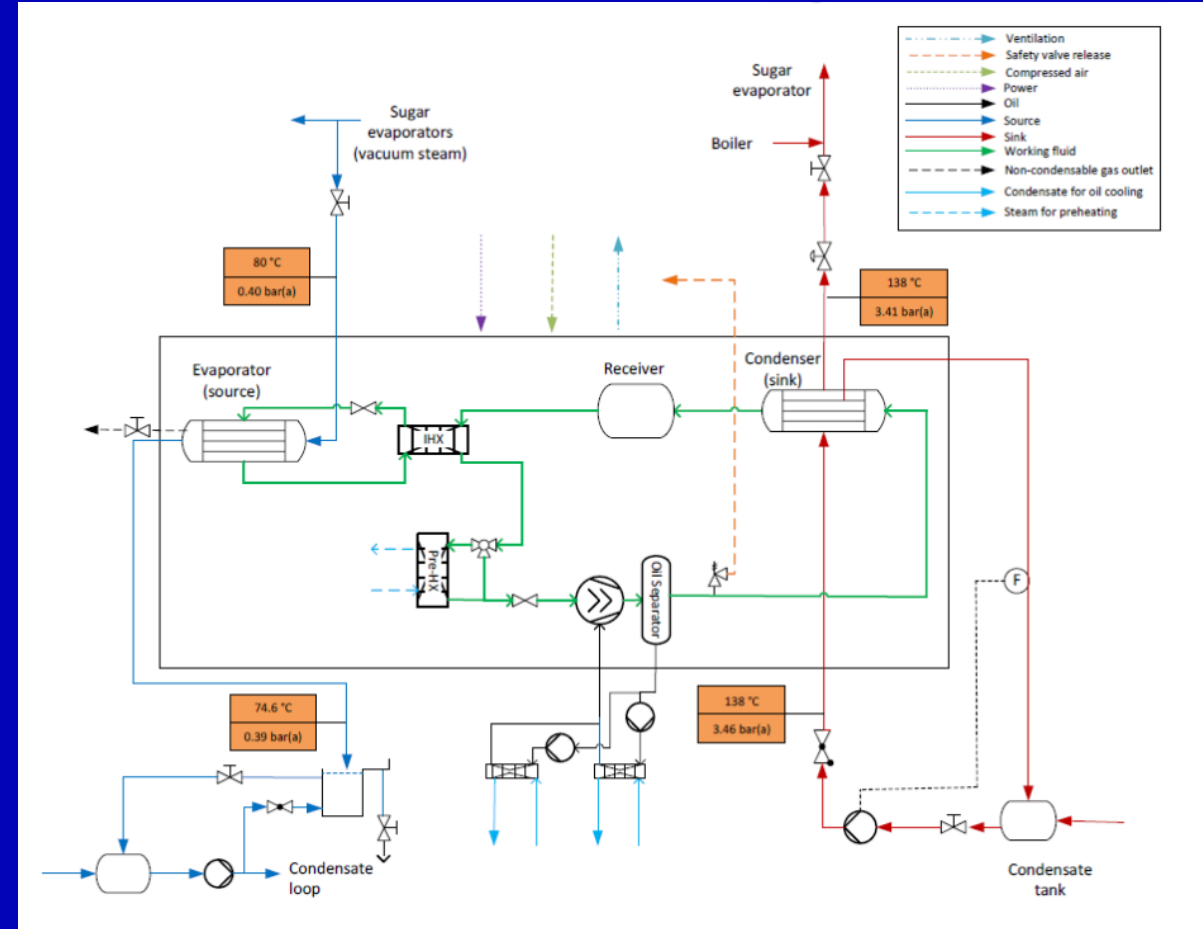
- Sugar production from sugar beets
- Focus on thick juice by evaporation of water

**Technology**

- Vapor compression heat pump
  - Pentane + screw compressor
  - Latent heat streams on source and sink

**Location: Tienen, Belgium**

This project has received funding from the European Union's Horizon Europe research and innovation programme under grant agreement No. 101069672 (SPIRIT).



# MVR (Mechanical Vapor Recompression) (Recompress Steam) Open Type Heat Pump

## Vapor Recompression (MVR)

Steam generated at low pressure from closed-type heat pumps can be re-compressed by means of an MVR to increase in pressure and temperature

MVR can raise the pressure up to <275 psig), other combined technologies can go higher.

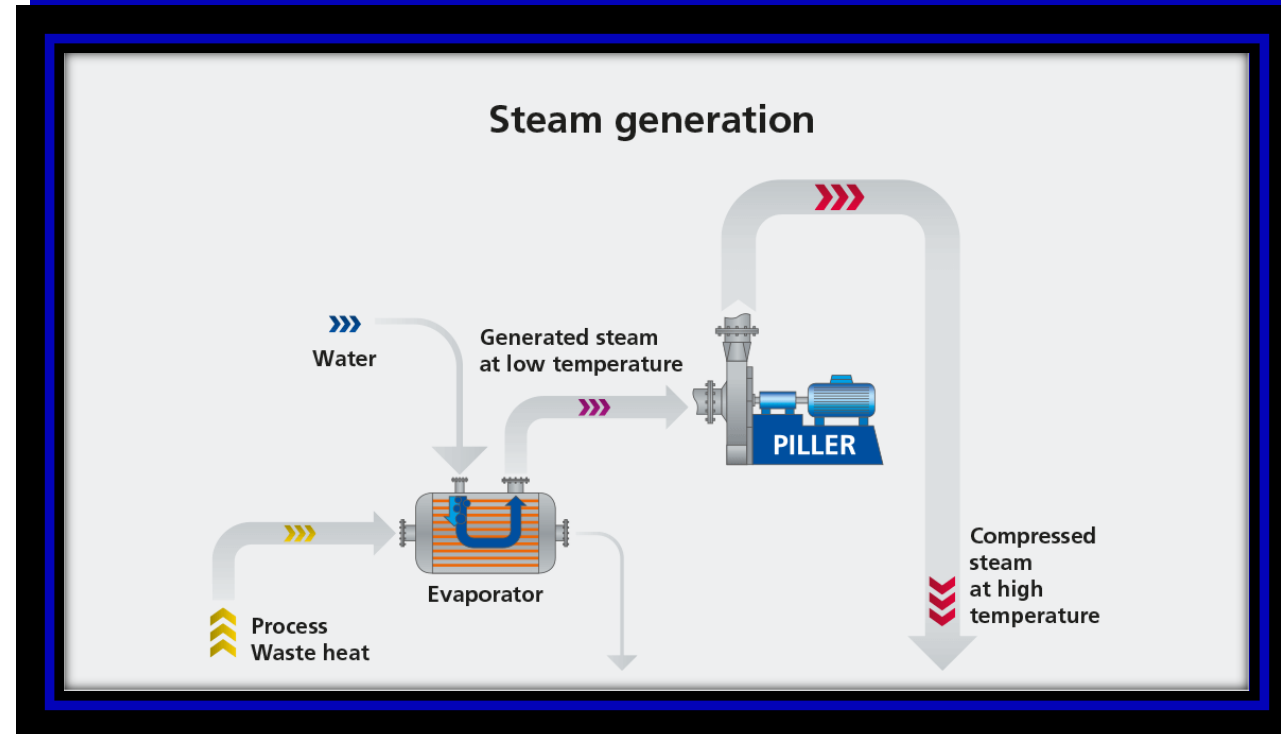
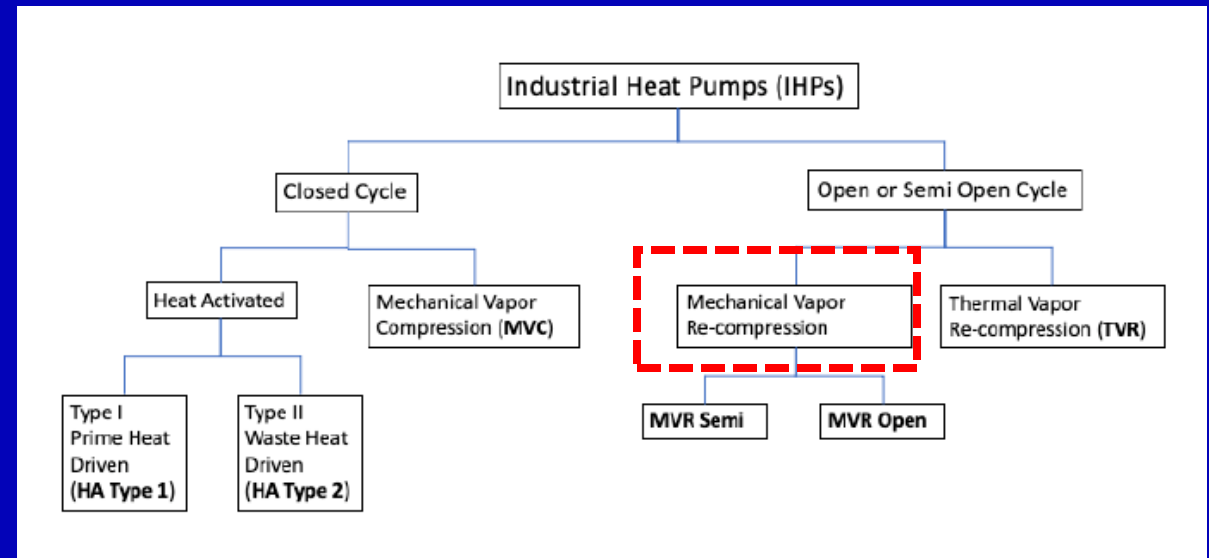
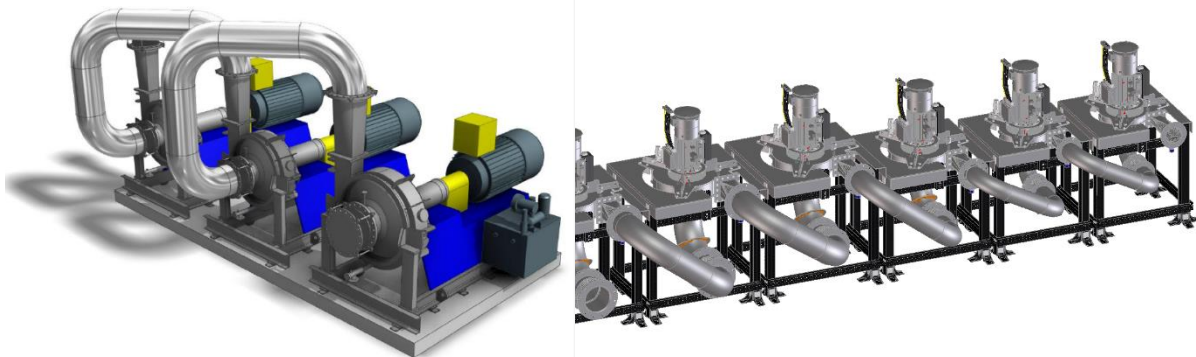
Typical Feed Temperatures at an MVR

120° F or 48.8° C

140° F or 60° C

170° F or 76° C

The higher the hot water inlet to the MVR, the better the COP of the MVR.





# VAPOR FANS – VACUUM STEAM RECOMPRESSION

## MVR – VAPOR FANS

Water has a change of state to Steam, in an exchanger or container that is in Vacuum (negative pressure)

Vacuum is created by the Steam Fan

Depending on conditions, each Steam Fan lifts on average 8°C to 10°C

Fan number or steps depends on final temperature

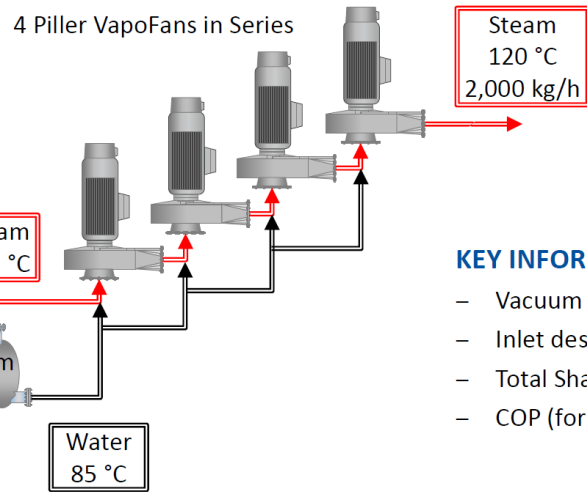
1st Fan lifts from 85°C + 10°C = 95°C

2nd Fan lifts 95 °C + 10 °C = 105 °C

3rd Fan Lifts 105 °C + 10 °C = 115 °C

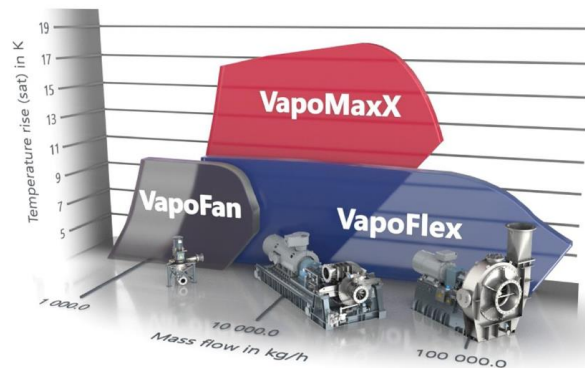
4th Fan Levant 115 °C +10 °C = 125 °C

4 Piller VapoFans in Series



### KEY INFORMATION

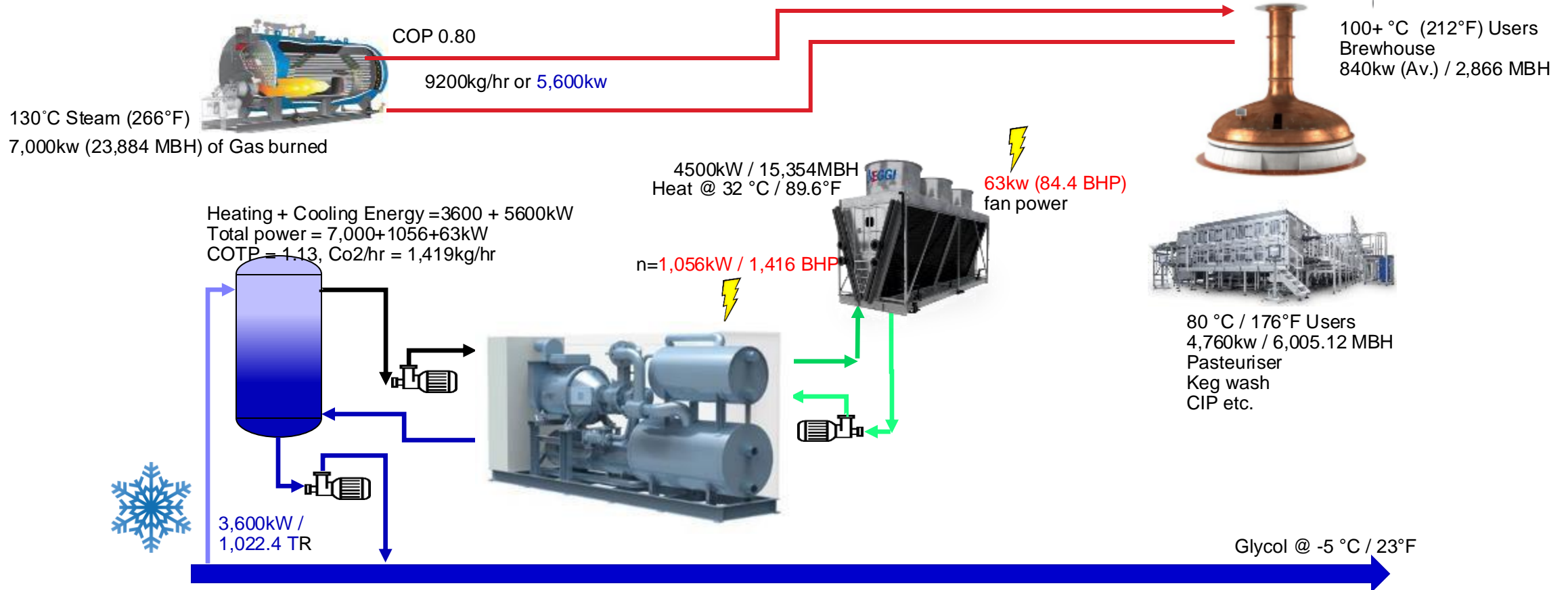
- Vacuum steam compression
- Inlet desuperheating
- Total Shaft Power: 189kW
- COP (for VapoFans Only): 6.02



Performance ranges for steam at 100 deg C inlet temperature

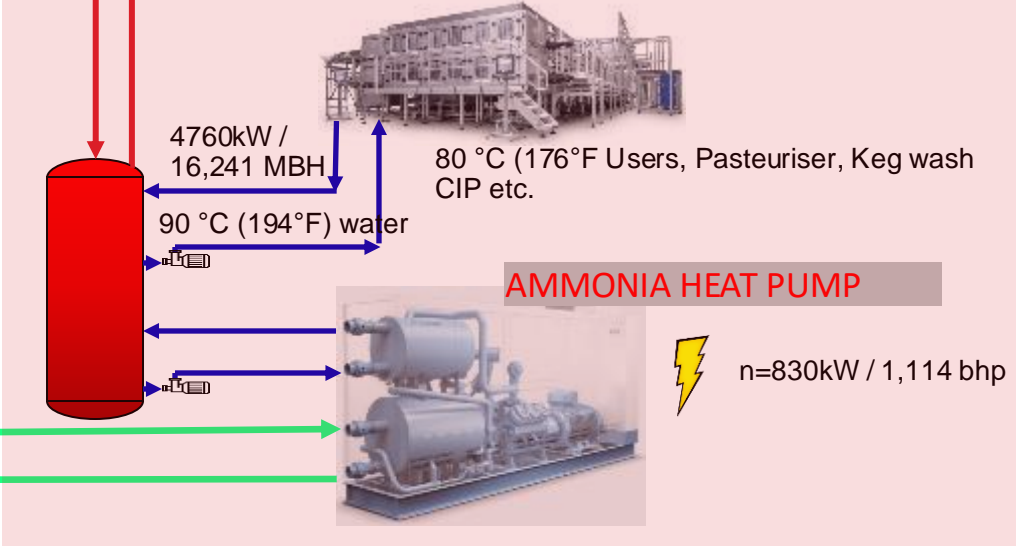
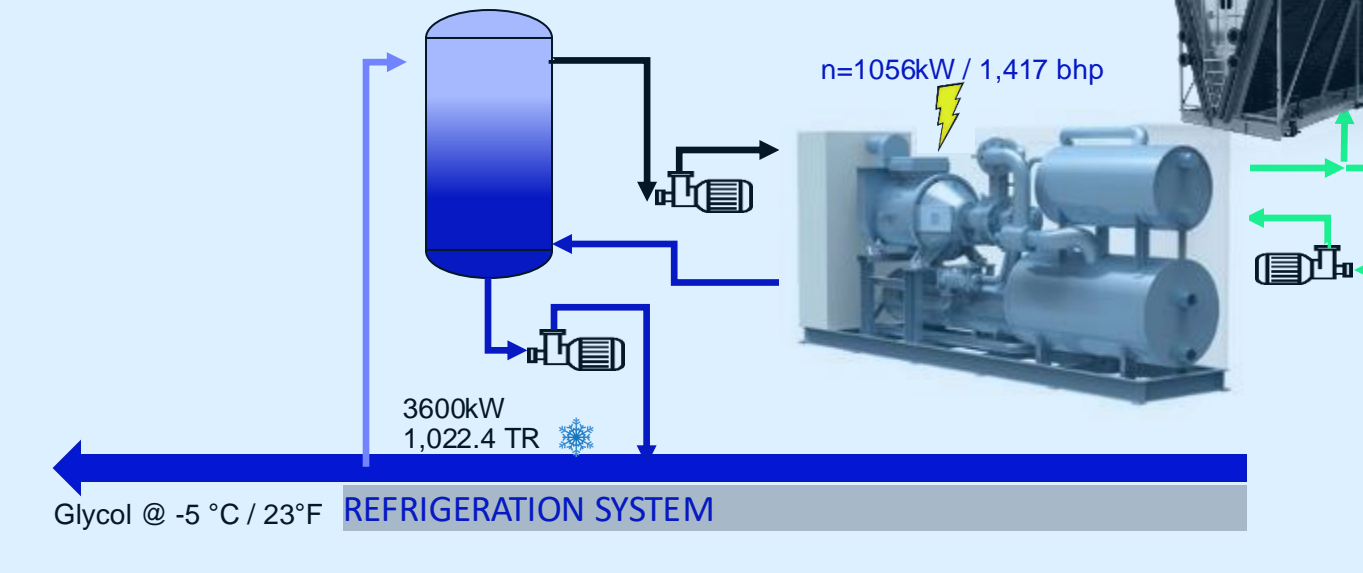
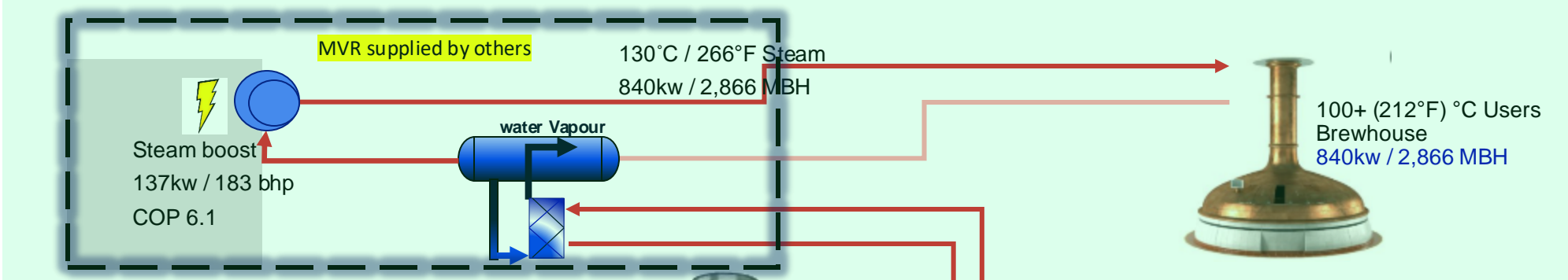
# The Norm in brewery

Boiler = Heat, Cooling = Cold



# Hot water and steam

Heating + Cooling Energy = 3600 + 5600kW  
 Total power = 137+1056+830kW  
 COTP = 4.5, Co2/hr = 158kg/hr





# The first steam-producing heat pump has been installed at Felleskjøpet Agri in Trondheim

- ✓ Produces 2 tons of steam per hour
- ✓ Recycles air-sourced waste heat
- ✓ Capacity of 1.4 – 1.8 MW<sub>th</sub>
- ✓ Efficiency gain of 67%

# STEAM TEMPERATURES ( CHILLERS + MVC+ MVR)

SCOPE OF SUPPLY

**Total Cooling capacity @ 2°C**  
13,320 kW  
**Total electrical power: 4500 kW**

**Total Heating capacity @ 85°C / 86°C**  
15,500 kW + 4780 kW = 20280 kW  
**Total electrical power: 3300 kW**

**MVR**

**Total Heating capacity @ 120°C**  
23,000 kg/h  
**Total electrical power: 1825 kW**

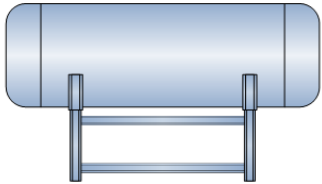
### CHILLERS

3 x LS Compressor – NH3  
XCR-XC2240-28  
Qo=4440 kW @3550rpm,  
Pe= 1500 kW

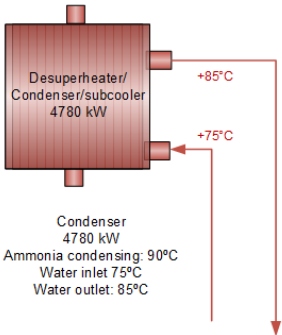
### AMMONIA HEAT PUMPS

Intercooler vessel  
50°C

6 x HS Compressor – NH3  
VXHP950  
Qc=3500 kW @1500rpm,  
Pe= 572 kW



Shell and tube cascade heat exchanger  
Heat transfer: 15,500kW  
Ammonia condensing: 90°C  
Water evaporating: 86°C, 0.6 bar



3 lines of Vaporfans – Steam  
Steam inlet: 7000 kg/h per line  
Steam outlet 7700 kg/h per line  
Pe= 608 kW per line

# ADD BETTER CONSULTING

SOSTENIBILIDAD



# Our organization

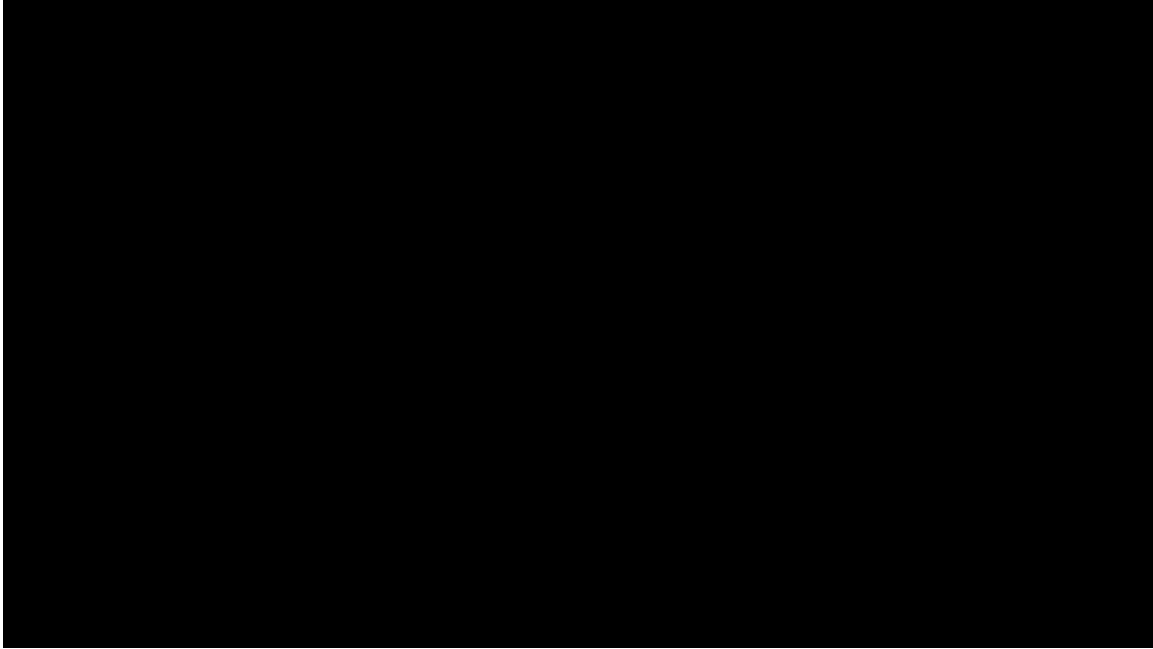
GEA is divided into **five divisions**, each with up to six business units. The units are based on comparable technologies and have leading market positions.

The **country organizations** stand ready to serve their respective customers as a central point of contact, offering them local access to an extensive portfolio of products and services.



# GEA NEXUS

Add Better: Holistic Solutions



GEA Expertise from all Divisions, incorporated to customer process



# BARRIERS of heat pumps



# WHY STILL SO HARD IN THE USA TO GET INTO A HEAT PUMP ??

**Despite the great ecological potential, there are still some market barriers to the wider spread of industrial HTHPs:**

**Lack in the understanding of the HTHP technology** (low level of awareness of the technical possibilities among users, consultants, investors, plant designers, producers, and installers).

**Lack of knowledge about the integration of HTHPs** in industrial processes.

**Cost-intensive integration into existing processes** due to tailor-made designs (leads to payback periods larger than for gas or oil-fired boilers).

**Lack of suitable and approved** compressors and refrigerants.

**Competing heat-producing technologies** generating high temperature using fossil fuels.

**Low fossil energy prices** (low gas to electricity price ratio)

**Lack of pilot and demonstration** systems.

**Lack of training and events** additionally supporting the spread of HTHP knowledge

**Domestic Manufacturing:** Not enough Manufacturers in the US and long lead delivery times ( 40 -50 weeks) ( Who holds the line are Heat Exchanger Manufacturers, they are in the 25-30 weeks lead time).

**Utility Pricing Structures** Currently utility demand tariffs are structured in such a way that drawing load during peak hours contributes to making electricity a non-competitive input fuel, compared to natural gas.

**Insufficient Grid Infrastructure** Infrastructure to support the requisite load of electrifying process heat is typically inadequate, including both distribution infrastructure and customer substation and internal wiring.

**What makes the USA different from Europe:**

Spark Gap or Spark Spread ( gas prices & kw prices) are much higher in EU which helps justify the energy savings and pay back

USA does not have yet a CO2 Emission Tax where in EU this factor justify many Heat pumps rather that Spark Gap ratio and Energy Savings.

Europe has learned to switch from Steam to Hot Water

EU has more Gov Funding than US.

# MANY BROWNFIELDS – RETROFITS DO NOT HAVE SPACE FOR HP

## CURRENT BARRIERS

### SPACE on BROWN FIELDS - RETROFITS

Many companies do not have space in their current Engine Room or Plant.

### OUTDOORS

This will force a market for **ENCLOSURES**

**ENCLOSURES** becomes Engine room so now it needs to follow all Codes, Fire Codes and any building code related to space, building



# TES ( Thermal Storage Energy) – Buffer Tanks

## TES ( WATER TANKS)

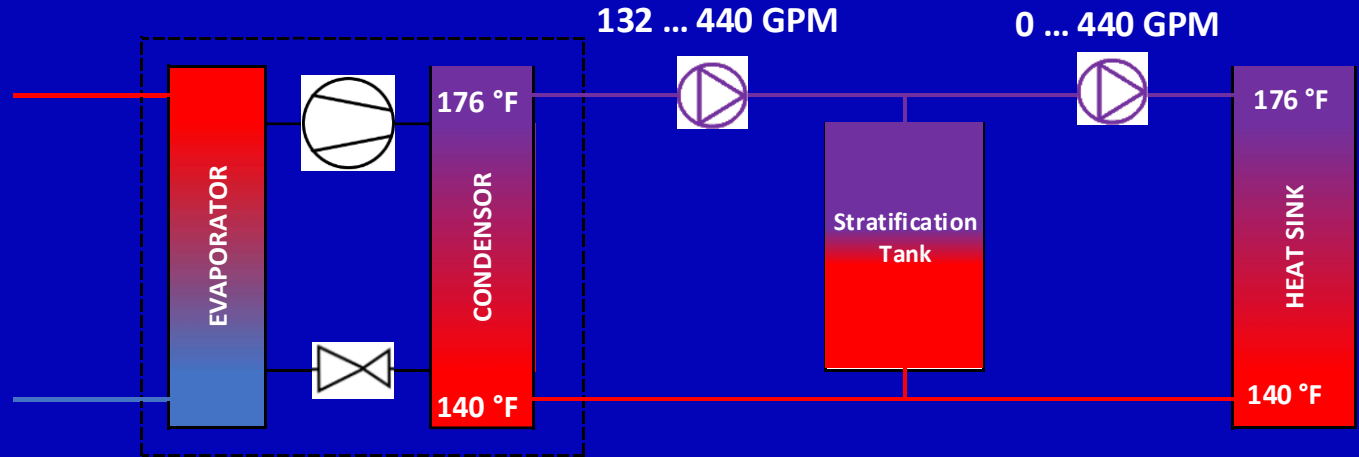
Handles better:

Partial load

Spikes

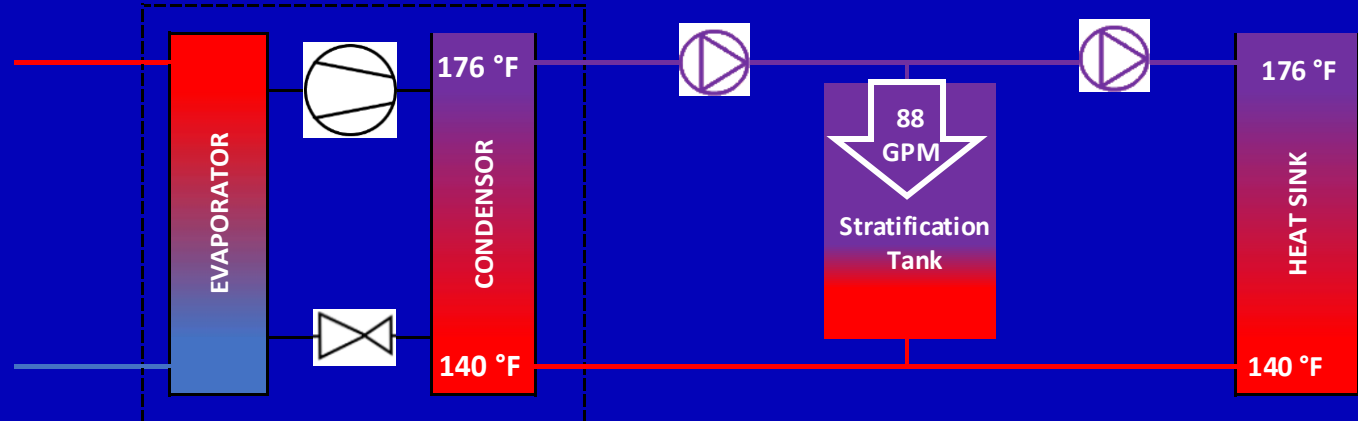
Sudden changes

Provides a more steady / stable operation



Heat pump can only operate  
30 ... 100%

Heat sink required to operate  
0...100 %



**The Dutch Coca-Cola factory  
has received CO2-neutral certification  
according to PAS2060**

**GEA** Engineering  
for a better  
world.